



EUROPEAN
COMMISSION

Community Research

RAPHAEL

Contract Number: **516508 (FI6O)**



DELIVERABLE (D-ST1.4)

Report on the He-FUS3 loop and experimental results for the system codes benchmarking exercise.

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Reporting period: 15/04/2007 – 15/04/2008

Date of issue of this report : 10/04/2008

Start date of project : **15/04/2005**

Duration : **48 Months**

Project co-funded by the European Commission under the Euratom Research and Training Programme on Nuclear Energy within the Sixth Framework Programme (2002-2006)

Dissemination Level

PU	Public	
RE	Restricted to the partners of the RAPHAEL project	X
CO	Confidential, only for specific distribution list defined on this document	

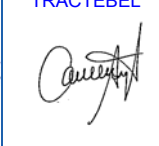
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[illegible]

ReActor for Process heat, Hydrogen And ELelectricity generation (RAPHAEL)		
Sub-project: SP-ST Work package: 4	RAPHAEL document no: RAPHAEL-0705-D-ST1.4	Document type: D=Deliverable
Issued by: : ENEA (I) Internal no.: FPN – P9L7-001		Document status: Final

Document title						
HE-FUS3 Loop: Data Sheets for Code Modelling and Experimental Data for Code Assessment						
Abstract						
This report contains a detailed description of the HE-FUS 3 helium loop and of the experimental tests performed to assess its performances in steady state and transient conditions. Moreover, all the experimental data acquired during the tests are enclosed to this report. The report, which is issued within the framework of the SP Safety (WP1) of RAPHAEL for the organization of a benchmark exercise aimed at the validation of the system transient analysis codes for VHTRs, has the purpose to provide the benchmark participants with the needed information for the HE-FUS 3 loop modeling, as well as to offer the data for code-to-experiment comparisons. In particular this revision 1 of the report would try to collect and answer some questions arisen within the benchmark participants during their earlier attempts to develop the loop model by providing an errata corripge and some integrative information.						
Revisions						
Rev.	Date	Short description	Author	WP Leader	SP Leader	Coordinator
1	10/04/2008	Data of the HE-FUS3 loop for benchmark exerciseData of the HE-FUS3 loop for benchmark exercise	M.Polidori P. Meloni (ENEA) 	Walter Van Hove SUEZ-TRACTEBEL 	Carmen Angulo SUEZ-TRACTEBEL 	Edgar Bogusch AREVA NP 

HE-FUS3 Loop: Data Sheets for Code Modelling and Experimental Data for Code Assessment

Analisi incidentale

In particular this revision 1 of the report would try to collect and answer some questions arisen within the benchmark participants during their earlier attempts to develop the loop model by providing an errata corrige and some integrative information.

Note: DRAFT version

In carico a:

2			NOME			
			FIRMA			
1	Revisione Generale Documento		NOME	M. Polidori	P. Meloni	R. Tinti
			FIRMA			
0	EMISSIONE		NOME	M. Polidori	P. Meloni	R. Tinti
			FIRMA			
REV.	DESCRIZIONE	DATA		REDAZIONE	CONVALIDA	APPROVAZIONE

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Errata Corrigé

Page 7, §2.2.1, Tab. 2 – The diameter of Line E is 4” instead of 5” and the maximum temperature of Line G is 420°C instead of 530°C.

Page 9, §2.3.1, Tab. 3 – The overall heat transfer surface is 5.09 m² instead of 4.52 m², the diaphragm pitch is in mm not kW, added the diaphragm diameter and thickness.

Page 9, §2.3.2, Tab. 4 – The vessel inside diameter is 800 mm instead of 880 mm, the vessel total height is 6638.2 mm instead of 7250 mm.

Page 10, §2.3.3, Tab. 5 – The overall heat transfer surface is about 27 m² instead of 27.7 m², the vessel active length is 4920 mm instead of 5000 mm, added diaphragm diameter and thickness and the tubes support plate thickness. Changed 3/8” tube outside diameter and the thickness of 1/2”, 3/8” ones.

Page 13, §2.3.7 – Added the valve flow coefficient dimension.

Page 19, §2.6.2, Tab. 13 – The rock wool conductivity is 0.045 instead of 0.04 W/m/K.

Figures – The overall figure numbing is revised.

Added figures:

- Fig. 6 – Electrical Heater Active Rods and Diaphragms Scheme
- Fig. 11 – 7-pin Test Section – Upper Part
- Fig. 14 – Test section Grid
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Figure 7 (Fig. 6 in Rev0) – Changed the Section A-A and added a particular that show the correct layout and dimension of the economizer diaphragms and tubes support plate.

Figure 11/13 – More Test Section dimensional information.

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Appendix A,

- Line B* – Insulator thickness 100 mm instead of 160 mm.
- Line C+P* – Insulator thickness 60 mm instead of 160 mm.
- Line D* – Insulator thickness 60 mm instead of 160 mm.
- Line F* – Maximum temperature 530 °C instead of 457/494 °C.
- Line G* – Maximum temperature 420 °C instead of 530 °C.
- Line H* – Insulator thickness 100 mm instead of 160 mm.
- Line H* – Maximum temperature 240 °C instead of 140 °C.
- Line I* – Insulator thickness 100 mm instead of 160 mm.
- Line I* – Maximum temperature 140 °C instead of 530/335 °C.
- Line L* – Maximum temperature 420 °C everywhere.

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1. Introduction

HE-FUS 3 is a helium facility that was designed and constructed at ENEA CR Brasimone in mid 90's for the thermal-mechanical testing of prototypical module assemblies of the DEMO reactor. At the end of the nineties a testing program, including steady state, cycling and transient tests was carried out on the facility in order to qualify its capability to perform experimental test campaigns both in normal and off-normal conditions.

Within the frame of the SP Safety (WP1) of the RAPHAEL Integrated Project, ENEA has offered these experimental data for the organization of a benchmark exercise aimed at the validation of the system transient analysis codes for Very High Temperature Reactors (VHTR). Although the loop characteristics are not prototypical of a Very High Temperature Reactor, the HE-FUS3 tests are useful to assess the capability of the codes to deal with a helium loop implementing a wide range of components such as compressor, pressurizer, pipes, diffusers, valves, heaters, heat exchangers and an active test section, and to model both steady-state and transient flows.

The experimental data make available for the benchmark, which are described in detail and completely enclosed to this report, are related to 10 steady state tests for the thermal-hydraulic characterization of the loop, 2 LOFA transients and a test campaign for the characterization of the helium compressor. The report also provides a detailed description of the HE-FUS 3 loop in order to support the participants in the benchmark for the loop modeling in their own codes

2. Facility Description for Code Modeling

2.1 General description

Within the frame of the European Fusion Technology Program, ENEA in 1993 obtained an economic support from EU for the construction of a helium facility, called HE-FUS3 [1]. The facility, which had been planned for the thermal mechanical testing of prototypical module assemblies for the DEMO reactor, was chosen for the selected European Helium Cooled Pebble Bed (HCPB) Blanket design to be tested on ITER reactor. The facility, also defined as the European Helium Cooled Blanket Test Facility, is located at the ENEA Brasimone Laboratories in Italy.

Its eight loop configuration [2], shown in Fig. 1, supplies the helium flowrate to an experimental Test Section, where the mock-up of the HCPB Blanket can be tested. The purpose of the eight-shaped closed loop arrangement is to separate two zones at different temperatures, the cold one including the compressor and the hot one the Test Section. An economizer, placed at the crossover point, recovers the gas enthalpy before recirculating the helium through the compressor. Thereby it has been possible to reduce both the need for external power to get the required temperature at the Test Section inlet and the cooler size to reduce the compressor inlet temperature to the level of its maximum continuative operating temperature. The main performances expected for the facility are reported in Tab. 1.

Parameter		Design Value
Max Pressure	MPa	10.5
Max Temperature	°C	530
Inlet Compressor Max Temperature	°C	100
Compressor Helium Flow Rate	kg/s	0.5-0.35
Max Compressor Speed	rpm	18000
Max Compressor Head	MPa	0.5
Compressor Electrical Power	kVA	136
Heaters Electrical Power	kW	210
Economizer Thermal Power	kW	564
Air-Cooler Thermal Power	kW	280
Helium Tank Capacity	m ³	3
Test Section Electrical Power	kW	350

Tab. 1 – HE-FUS3 Main Performances

The loop components relevant for the code modeling are (Fig. 2):

- Main Piping in AISI 316, 4”-5” (sch. 80);
- regenerative compressor with pneumostatic helium shaft supporting system;
- three modules of a flanged immersion rod bundle electrical heater;
- tube-shell helium-helium economizer;

- air cooler with finned tubes;
- expansion tank ;
- two mixers to make uniform the temperatures of the main and by-pass flowrate in cold and hot zone;
- three global valves for the regulation;
- 7-pin bundle electrically heated Test Section.

Operation and control of the system are guaranteed through several auxiliary systems which are not relevant for the modeling: passive safety system, filling and pressure control system, vacuum preservation system, gas analysis and facility control system. The loop is also provided with on/off valves for the control.

2.2 Loop Piping

2.2.1 Piping Layout

The piping overall length is about 80 m, with an integral volume of 4m³ including 3m³ of the expansion tank and a weight of about 15 ton. The diameters of the main pipes were preliminary fixed at 4" (sch. 80) for the cold zone et 5" (sch.80) for the hot zone in order to limit at 20 m/s the helium velocity in the loop. The piping material is stainless steel AISI 316. Contact temperatures are reduced below 50 °C by means of heat insulator with special asbestos-free material, 60 to 160 mm in thickness.

The main characteristics of the different lines constituting the piping are reported in Tab. 2. A 3D sketch of the piping layout reported in Fig. 3 allows visualizing the relative position of the lines.

Line	Description	Diameter (inch)	Wall Thickness	Insulation Thickness (mm)	Max Temp (°C)
A	From TS to Economizer	5"	Sch. 80	160	520
B	From Economizer to Air-cooler	4"	"	100	240
C	From Air-cooler to Compressor	4"	"	60	100
D	From Tank to Cold By-pass T	4"	"	60	140
E	From Economizer to Heater 3	4"	"	160	420
F	From Heater 3 to Heater 1	5"	"	160	530
G	From Heater 1 to TS	5"	"	160	420
H	From Cold By-pass T to Economizer and Cold By-pass	4"	"	100	240
I	By-pass TS	4"	"	100	140
L	By-pass Heater 3-2	4"	"	160	420
P	From Compressor to Tank	1"½	"	60	100

Tab. 2 – HE-FUS3 Lines Main Characteristics

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2.2.1 Piping runs and volumes

In order to support the description of the facility in the different T/H codes, in attachment A is reported the noding of the loop used for the thermo-mechanical analysis. The different lines refer to the piping layout in Fig. 3. Both pipes and components are included. For each node the following information are listed:

- The type of hydraulic element used (Straight Element, Curve Element, Bending Center, T-Shape Element)
- 3D Cartesian coordinates
- Node number
- Pipe outside diameter
- Pipe thickness
- Insulator thickness

A schematic representation of the pipe runs is also reported for each line.

2.3 Major Components

Quite detailed information is provided for each of the major component listed in sub. 2.1. This information provided with tables is mainly related to the geometrical data and thermo-hydraulic characteristics because it is addressed to T/H code modeling. Some reproductions of the as-built designs are also reported, where available, in order to provide further geometrical details.

2.3.1 Electrical Heaters E219-1/2/3

The electrical heater is subdivided in three identical modules each of them constituted by a bundle of 30 U-bent active rods immersed in a vertical cylindrical pressure vessel. The rods are made of Ni-Cr spiral wire electrical resistors insulated by MgO compressed powders in AISI 316 cladding to reach the nominal diameter. The pin cold legs are welded to an upper plate, flanged to the vessel, by interposing tubes for the welding accommodation. The rod bundle is provided by diaphragm plates for the heat transfer improvement.

The nominal power supply is 210 kW (70 kW per module). The electrical supply, control and monitoring is independent for each module. The hydraulic configuration of these three modules can be changed by means of manual valves HV 250, HV 251, HV 252 (Fig.1):

- a module serial configuration to supply a Test Section with the whole power
- use of recycling lines to supply a TS with 1/3 (1 module) or 2/3 (the other two modules) of power

The electrical supply is 380 V three-phase at 50 Hz. In the last two modules (E219-1/2) the electrical power is controlled by an SCR controller using as a signal the helium temperature at the outlet of each vessel. Instead the first module is manually actuated with on-off regulation. The main design parameters are reported in Tab. 3. Further geometrical details can find in the as-built drawings from Figs. 4 to 6.

Parameter		Design Value
Nominal Helium Inlet Temperature	°C	420
Nominal Helium Outlet Temperature	°C	525
Design Helium Temperature	°C	530
Design Cladding Temperature	°C	560
Design Helium Pressure	MPa	10.5
Design Helium Flowrate	kg/s	0.35
Electrical Power	kW	70
Overall Heat Transfer Surface	m ²	5.09
Overall Thermal Conductance	W/m ² K	809
Design Pressure Drop	Pa	1011
Rod Diameter	mm	15
Nr U-bent Rods		30
Rod Heated Length	mm	1800
Rod Cold Leg Length	mm	300
Nr of Diaphragm Plates		12
Diaphragm Pitch	mm	145
Vessel Internal Diameter	mm	270
Diaphragm Diameter	mm	268
Diaphragm Thickness	mm	3

Tab. 3 – Heater Single Module Main Design Parameters

2.3.2 Expansion vessel

An expansion vessel is located at the compressor outlet, in order to dump pressure and flow fluctuations during loop operation. The vessel is an 8 m high vertical cylinder with a volumetric capacity of 3 m³. It is provided with several connections to the loop: two for inlet/outlet main flow, one to the outlet purification circuit, one from the filling and pressurizing line, one for the controlled flow discharge to the environment, the last one for the passive safety rupture disk. The main design parameters are reported in Tab. 4.

Parameter		Design Value
Max Design Pressure	MPa	10.5
Max Design Temperature	°C	160
Maximum Design Flowrate	kg/s	0.35
Vessel Capacity	m ³	3
Vessel Outside Diameter	mm	890
Vessel Inside Diameter	mm	800
Vessel Total Height	mm	6638.2 ^(*)

(*) Because of the uncertainties in the real vessel capacity consider this value as reference for the benchmark.

Tab.4 – Expansion Vessel Main Design Parameters

2.3.3 Economizer E214

This component is a high efficiency (>79%), tube shell geometry, helium/helium heat exchanger with vertical axis. The hot helium coming from the Test Section flows through a bundle of straight tubes that are welded between two tube plates and immersed in a cylindrical pressure vessel. The cold helium counter-flows in the shell zone where a series of diaphragm sheets allow improving the global thermal exchange. The tube bundle is floating respect to the shell by a tube-below compensation system. The pressure vessel is cylindrical and is provided with four welded pipes for the loop connections.

The main design parameters are reported in Tab. 5. Further geometrical details can find in the as-built drawing in Fig. 7.

Parameter		Design Value
Cold Helium Inlet Temperature	°C	130
Cold Helium Outlet Temperature	°C	440
Hot Helium Inlet Temperature	°C	530
Hot Helium Outlet Temperature	°C	220
Maximum Design Pressure	MPa	10,5
Cold Side Pressure Drop	Pa	1660
Hot Side Pressure Drop	Pa	212
Overall Heat Transfer Surface	m ²	27.0
Overall Thermal Conductance	W/m ² K	258
½" Tube Multiplicity		73
½" Tube Outside Diameter	mm	21.3
½" Tube Thickness	mm	1.65
3/8" Tube Multiplicity		12
3/8" Tube Outside Diameter	mm	17.2
3/8" Tube Thickness	mm	1.65
Vessel Active Length	mm	4920
Diaphragm multiplicity		18
Diaphragm Thickness	mm	3
Diaphragm Diameter	mm	266
Tubes Support Plate Thickness	mm	23

Tab. 5 – Economizer Main Design Parameters

2.3.4 Compressor K200

The prototypical compressor developed by RTM company has the electrical motor completely immersed in the helium flow. The regenerative impeller has a shaft bearing system based on pneumostatic helium control of the support clearances, without using any lubricant. In order to control the diametric bearing clearance values in the range of 40 µm, a helium flow is injected through calibrated nozzles in the gaps between the shaft and the bearing at the required pressure. The electrical motor is provided with an inverter driving system capable of controlling the frequency in the range 5-300 Hz, driving the rotor speed at 300-18000 rpm.

A special ancillary circuit provides for helium pressure injection flow in the pneumostatic ring and for the flow necessary to cool the electrical motor internally. Both these helium auxiliary

flows are derived from the compressor outlet at 140 °C (nominal conditions), cooled at room temperature by a two stage water heat exchanger, and then reintroduced at the compressor inlet. More exhaustive information about the characteristic of this derivative flow will be given in chapter 3.

The maximum compressor inlet temperature is fixed at 100 °C in order to control and maintain the nominal bearing clearances at acceptable value.

The main design parameters are reported in Tab. 6. Further geometrical details can find in the as-built drawing in Fig. 8.

Parameter		Design Value
Maximum Design Helium Temperature	°C	160
Maximum Design Helium Pressure	MPa	10.5
Design Flowrate	kg/s	0.05 -0.35
Vessel Inside Diameter	mm	350
Vessel Sheet Thickness	mm	45
Vessel Total High	mm	700
Inlet Design Pressure	MPa	6.0
Outlet Design Pressure	MPa	6.5
Maximum Design Flowrate	kg/s	0,35
Maximum Design Inlet Temperature	°C	100
Mechanical Power	kW	90
Electrical Motor Power	kVA	110
Maximum Inverter Current	A	210
Maximum Inverter Frequency	Hz	400
Impeller Maximum Speed	rpm	18000
Impeller Diameter	mm	230
Motor Shaft Diameter	mm	65
Rotor Diameter	mm	130
Diametrical rotor Clearances	mm	1
Bearing clearances	µm	40

Tab. 6 – Compressor Main Design Parameters

2.3.5 Air Cooler

This component is located at the compressor inlet in order to reduce the corresponding helium temperature below the maximum design value (100°C). It is a counter flow helium-air heat exchanger, where the helium flows inside the tube bundle whilst the air flows outside the external surface of the tubes. A helicoidal stainless steel sheet is welded on the outside surface of the tube to increase the overall thermal conductance. The bundle arrangement is as compact as possible with the finned tubes in a triangular array and welded to two cylindrical distributors.

The air flow is pumped from a fan that is controlled by an SCR using as a signal the helium temperature at the air cooler outlet.

The main design parameters are reported in Tab. 7. Further geometrical details can find in the as-built drawing in Fig. 9.

Parameter		Design Value
Nominal Helium Inlet Temperature	°C	240
Nominal Helium Outlet Temperature	°C	100
Design Helium Temperature	°C	240
Design Helium Pressure	MPa	10.5
Design Helium flow rate	kg/s	0.35
Design Helium Pressure Drop	Pa	4000
Nominal Air Inlet Temperature	°C	30
Nominal Air Outlet Temperature	°C	70
Design Air pressure	MPa	1
Design Air Flowrate	kg/s	6.1
Design Air Pressure Drop	Pa	1200
Nominal Thermal Power	kW	280
Overall Heat Transfer Surface	m ²	165
Overall Thermal Conductance	W/m ² K	400
Nr of ½" Finned Tubes		22
Finned Tube Outside Diameter	mm	21.3
Fin thickness	mm	0.4
Fin pitch	mm	3.4
Fan Electrical Power	kW	15
Fan Speed	rpm	50-3000

Tab.7 – Air Cooler Main Design Parameters

2.3.6 7-Pin Test Section

The original dummy Test Section, already used for the acceptance test of the facility, was replaced in 1997 this new actively heated test section. This new TS consists of a 7-pin bundle 50 kW of nominal power each, contained in a pipe, which is inserted from the flanged bottom end in the tubular pressure vessel of the dummy mock-up. The bundle is appropriately equipped with thermocouples in order to monitor the transient temperature field during the accident simulations planned in the facility.

The heated pins are made of Ni-Cr spiral wires insulated by MgO powders with a Ni-Fe-Cr alloy cladding. The helium enters in the annular space between the tubular pressure vessel and the TS pipe, flows down to the TS inlet then flow up within the pipe around the pins.

The main design parameters are reported in Tab. 8. Further geometrical details can find in Figs. 10 to 15.

Parameter		Design Value
Nominal Helium Inlet Temperature	°C	420
Nominal Helium Outlet Temperature	°C	525
Design Pressure	MPa	20
Effective Power per Rod	kW	40
Max Cladding Temperature	°C	950
Max Heat Flux	W/cm ²	110.6
Heated Length	mm	2000
Rod Diameter	mm	9.5
Clad thickness	mm	1
TS Pipe		1 ½" (sch.10)
Mock-up Tubular Vessel		3" (sch. 80)

Tab.8 – 7-pin TS Main Design Parameters

2.3.7 Valves

The loop is provided with a series of valves for regulation, flow configuration and safety control (Fig. 1). The regulation valves for the main flow FV 213, FV 234, FV 235 and FV 10 are globe valves with metallic bellows tightness, pneumatically actuated and with a steam opening indicator system. For the flow configuration and safety control there are also 5 on/off valves with a manual or pneumatic actuation and open/close indicator system that are not relevant for the loop simulation. The data sheets of regulation and on/off valves are listed in Tab. 9.

A technical communication related to the regulation valve FV 213, FV 234 and FV 235 reports a value of 27 for the Flow Coefficient (Cv) at 100% opening, moreover it states that 10% opening is the minimal value for their regulation. The characteristic of the regulation valves (Flow Coefficient vs. Stroke) reported in Fig. 16 have been drawn from the same communication.

For a correct use of the information above it is worth to remind that the following correlation is used for valve sizing at sub critical gas flow conditions:

$$W = 355C_v \sqrt{\frac{G\Delta P(P_1 + P_2)}{T}}$$

W = Weight flow rate [Kg/h]

Cv = Valve flow coefficient [USgpm of water with ΔP=1 psi]

G = Gas specific gravity (air=1)

$$G = \frac{\text{Helium Molecular Weight}}{\text{Air Molecular Weight}} = \frac{4.0026 \text{ [g/mol]}}{28.96443 \text{ [g/mol]}} = 0.13819$$

ΔP = Valve pressure drop [bar]

P₁ = Valve upstream pressure [bar abs]

P₂ = Valve downstream pressure [bar abs]

T = Upstream absolute gas temperature [K]

Nr Valve	Builder	LINE	Ø	operation
FV 213	NUOVO PIGNONE	D	1 ½"	Regulated
FV 234	"	I	1 ½"	"
FV 235	"	H	1 ½"	"
FV 10	"	C	1 ½"	"
HV 2	"	P	1 ½"	ON/OFF
HV 250	"	E	3"	"
HV 252	"	F	4"	"
FV 230	ABB	G	4"	"
FV 231	ABB	A	4"	"

Tab.9 –Main Valves Data Sheet

2.3.8 Mixers

Two mixers are used in the loop for the temperature mixing between different main and by-pass flow rates. They are constituted by two annular tubes, with the internal one drilled and provided with sliding pads, assembled in order to avoid the relative temperature stress accumulation on the welding zones. These mixers are welded to the pipelines.

The cold mixer is located between the by-pass line and the economizer outlet to guarantee the thermal mixing between the hotter branch, coming from the economizer outlet, and the colder one, coming from the cold by-pass line.

The hot mixer is located between the TS by-pass line and the last heaters outlet to guarantee the thermal mixing between the hotter branch, coming from the last heater outlet, and the colder one, coming from the hot by-pass line.

The main design parameters for the two mixers are reported in Tab. 10. For geometrical details one can refer to the as-built drawing in Fig. 17.

Parameter		Design Value
Cold Mixer		
Nominal Cold Helium Temperature	°C	130
Nominal Hot Helium Temperature	°C	220
Design Helium Pressure	MPa	10.5
Design Helium Flowrate	kg/s	0.35
Hot Mixer		
Nominal Cold Helium Temperature	°C	130
Nominal Hot Helium Temperature	°C	530
Design Helium Pressure	MPa	10.5
Design Helium Flowrate	kg/s	0.35

Tab.10 – Mixers Main Design Parameters

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2.4 Instrumentations and control chains

The instrumentation map of the facility is shown in Fig. 18. In the following paragraphs is given a description of the instrumentation installed in the main loop [2].

2.4.1 Flow measurements

The two flow controllers in the main line, FT 212 and FT 228, are based on the volumetric flow measurements with 2 Vortex flow meters of 2". In order to compute the mass flowrate, the volumetric flow signal is integrated with measurements of the temperature and pressure upstream of the flow meter location.

The flow transmitters give a correct measurement at a flow rate less than 5% of the measuring range. The measurement elements of the transmitter are located at least 10 diameters upstream and 5 downstream of uninterrupted pipe length for better measurement accuracy. Thus, the accuracy results better than 0.5% of the true value for a flow rate above 10% of its range.

2.4.2 Temperature measurements

The temperature sensors are thermocouples ANSI K (NiCr/NiAl) for temperature values higher than 200 °C and Platinum Thermoresistances ANSI PT 100 for lower temperature values. The accuracy is better than 0.5% on the measuring point.

The thermocouple wire insulator is MgO, and the cladding sheath is ANSI 316. The diameter of the outer thermocouple sheath is 3 mm. All the measurement points are provided with AISI 316 thermo wells welded to the pipes and with interchangeable fitting connections.

Only the thermocouples TT 222, TT 223, TT 232, TT 244 and TT 242, used for the regulation chains, are directly exposed to the fluid in order to monitor as rapidly as possible the real helium temperature. A response time close to 1 second can be considered for the thermocouples not directly exposed to the fluid. The temperature signals are locally compensated and linearized by transmitters.

2.4.3 Pressure measurements

The pressure measurements are based on diaphragm cell transmitters. Only one manometer, mounted on the expansion tank, is a Bourdon type without signal transmission.

All the pressure transmitters are provided with interception manifolds (5-way for differential transmitter). The accuracy of the gauges is better than 0.5% on the measuring point.

2.4.4 Control chains

The operator can manage, in local manual or automatic remote modes, the following six measurements and control:

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- TT 232 – Test Section inlet helium temperature with feedback control on the hot bypass valve FV 235;
- TTT 223 – Heater E 219/1 outlet helium temperature with feedback control on the relative SCR heater supply control;
- TTT 222 – Heater E 219/2 outlet helium temperature with feedback control on the relative SCR heater supply control;
- FT 212 – Compressor helium flowrate with feedback control on the relative inverter driving motor control;
- FT 228 – TS outlet helium flowrate with feedback control on the main control valve FV 213;
- TT 242 – Air cooler E 240 outlet helium temperature with feedback control on the fan inverter driving motor control.

Moreover, it is foreseen a protection system for the emergency shutdown of the facility, which is independent from the control system, based on the following signals:

- TT 236 - Heater E 219/1 outlet helium temperature;
- TT 297 - Heater E 219/2 outlet helium temperature;
- TT 241 - Air cooler E 240 outlet helium temperature.

2.5 Heat Losses and Pressure Drops

2.5.1 Heat Losses

A characterization of the heat losses along the loop based on experimental data is not available. The thickness of insulation material (rock wool) that was calculated to reduce contact temperatures below 50 °C, resulted in 160 mm in the hot zone of the loop and 60 mm in the cold one.

The heat losses distribution resulting by the design calculations [3] at the loop nominal conditions is reported in Tab. 11. According to these calculations the nominal heat losses are well lower than 20 kW that was the design performance. This evaluation seems extremely optimistic for two reasons:

- The conductivity of the rock wool used in the calculation (0.045 W/m°C) is typical for ambient temperature application, whereas its average temperature in the hot zone of the facility should be higher than 300°C. The conductivity increases rapidly with the temperature (e.g. 0.08 W/m°C at 300°C) and this fact should be taken into account in the new calculations (Fig.19).
- The thermal bridges related to mechanical junctions, instrument and electrical connection penetrations are not considered in the calculations.

These considerations suggest that the design calculations considerably under estimated the thermal losses in the design calculation. Further considerations on this subject will be made in next chapter.

Line/Component	Inlet Temperature (°C)	Linear Heat Losses (W/m)	Total Heat Losses (W)
From Compressor to Tank	140	43.69	27,09
Tank	139.98	199.72	882,77
From Tank to Economizer	139.49	43.51	500,39
Economizer	139.21	160,57	791,64
From Economizer to Heater 3	420	142.69	606,45
Heater 219/3	419.66	250.95	552,09
From Heater 3 to Heater 2	457.99	174.54	78,54
Heater 219/2	457.94	275.56	606,25
From Heater 2 to Heater 1	496.24	189.79	465,01
Heater 219/1	496.01	300.16	660,36
From Heater 1 to TS	534.34	204.97	1014,62
From TS to Economizer	533.78	204.75	286,65
From Economizer to Air-cooler	240	59,99	277,26
From Air-cooler to Compressor	100	19,35	34,84
Total			6783,96

Tab. 11 – HE-FUS3 Heat Losses Calculated at Nominal Conditions

2.5.2 Pressure drops

The directed measurements of the pressure drops are available only on two parts of the loop respectively including compressor and Test Section. Although they are the most relevant components for the pressure drops, that is insufficient for a complete characterization of the loop. Moreover, the pressure signals are not sufficiently accurate to be used to this purpose. In Tab. 12 is reported a numerical evaluation of the relevant pressure drops along the loop. It is worth drawing attention on the large pressure drops calculated through the valves FV-213 and FV10.

Component	Helium Velocity (m/s)	k	Pressure Drop (mbar)	Stroke %
Valve FV213 1 ½"	8.37	282.43	650	58.5
Valve HV252 3"	4.25	3.85	1.5	100
Valve FV 230 4"	4.58	3.81	2	100
Test Section Annular Part	15.32	15	71	
Test Section Inner Part	26.25	15	215	
Valve FV 231 4"	5.14	3.65	2	100
Flange FT228	28.35	7	161	
Mixer	5.58	5	4	
Filter Compressor Inlet	15.33	3	25	
Valve FV10 1 ½"	15.34	62.72	501	60.5

Tab. 12 – HE-FUS3 Relevant Pressure Drop Calculated at 0.225 kg/s, 50 bar at nominal temperatures

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2.5 Miscellanea

2.6.1 Helium Leakage

According to the design performance of the facility the helium leakage amount to 10^{-5} mbar l/s per component and $2 \cdot 10^{-3}$ mbar l/s for the whole facility.

2.6.2 Economizer Global Heat Exchange Coefficient

The thermal-hydraulic behavior of the loop both in steady state and transient conditions is very much depending on the efficiency of the economizer. Its correct evaluation is essential for the accuracy of the loop simulation with a T/H system code. In order to provide further information for the code modeling, the correlations used in the design calculations [4] for the heat transfer coefficients are reported in the following. It is interesting to notice that while the heat transfer coefficient tube side was calculated with the typical Dittus-Boelter correlation, in the shell side, where the presence of diaphragms improves the thermal exchange, a more suitable correlation was used.

$$q = (T_i - T_e) \cdot \pi D_e l \cdot U$$

$$U = \left[\frac{D_e}{D_i h_i} + \frac{D_e \cdot \ln(D_e / D_i)}{2 \cdot K_{steel}} + \frac{1}{h_e} \right]^{-1}$$

$$Nu = \frac{h_i D_i}{K_i} = 0.023 Re^{0.8} \cdot Pr^{1/3}$$

$$h_e = 0.36 \frac{K_e}{D_e} \cdot Re_{max}^{0.55} \cdot Pr^{1/3}$$

q	= Exchanged Power [W]
T_i	= Internal (Tube) Temperature
T_e	= External (Shell) Temperature
D_i	= Internal Diameter [m]
D_e	= External Diameter [m]
l	= Length [m]
h_i	= Tube Heat Transfer Coefficient [$W/m^2 \cdot K$]
h_e	= Shell Heat Transfer Coefficient [$W/m^2 \cdot K$]
U	= Global Heat Exchange Coefficient [$W/m^2 \cdot K$]
K_{steel}	= Steel Thermal Conductivity [$W/m \cdot K$]
K_e	= External Thermal Conductivity [$W/m \cdot K$]
K_i	= Internal Thermal Conductivity [$W/m \cdot K$]
Re	= Reynolds Number
Re_{max}	= Reynolds Number Calculated at Maximum Flow Area
Pr	= Prandtl Number
Nu	= Nusselt Number

2.6.2 Material Thermal Properties

The thermal property data related to some materials relevant for the T/H modeling of the facility, as used in previous works [5], are reported in Tab. 13.

Material	Temperature K	Conductivity W/m/K	Thermal Capacity J/m ³ K
AISI 316	273	13.851	4.06E06
	323	14.322	4.09E06
	353	14.793	4.12E06
	373	15.108	4.14E06
	473	16.679	4.20E06
	573	18.249	4.25E06
	673	19.821	4.28E06
	773	21.392	4.30E06
	873	22.963	4.34E06
	973	24.534	4.39E06
Rock Wool	273 - 973	0.045(*)	0.615E06
Magnesium Oxide	273 - 973	2.077	2.681E06

(*) Read page 16 §2.5.1

Tab. 13 – HE-FUS3 Material Thermal Property Data

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3. Experimental Data Description

The experimental data available for the assessment of the thermal-hydraulic codes were carried out for the characterization of the facility during the years 1998 and 1999. They include 10 steady state tests (Pressure 25÷50 bar, Helium Mass Flowrate 0.1÷0.227 kg/s, Power 50÷130 kW, Helium Max Temperature 310÷520 °C), 2 Loss of Flow transients and a test campaign for the characterization of the helium compressor (25 and 50 bar).

3.1 Steady State Tests

Most of the steady states were carried out at 50 bar of pressure on 24th and 25th of June 1998. They are identified with one digit number from 1 to 9, followed by ST for steady state and by the indication of the day (e.g. 24-06-98). Data from 8 tests are reported in this document because the recording for test nr 3 is not available.

Other 2 tests were carried out at 25 bar of pressure on 19th of February 1999. They are identified with a two-digit number indicating the power in % supplied by the Test Section, followed by ST for steady state and by the indication of the day (e.g. 19-02-99). In these tests the characteristics of the compressor are enough different from those of the previous tests owing to a new rotor mounted at the beginning of that year.

3.1.1 Facility Configurations

In the following for each test will be described the status of the loop in term of boundary conditions and status of the controls: pressure, mass flowrate, electrical power and way to supply it, active controls description.

1ST24-06-98 – This test was carried out at relatively low helium temperature and 50 bar pressure. The compressor operated at 13000 rpm to provide a quite high helium mass flowrate (0,222 kg/s). The electrical power was supplied by heaters E219/2 (26.6 kW) and E219/3 (40 kW) controlled by the corresponding helium outlet temperature. The control of the regulation valves FT 213, FT234, FT235 was not active. The main valve FT213 was completely open, whereas the by-pass valve FT234 and FT235 were closed.

2ST24-06-98 – The test was conducted at the same conditions and loop configuration as the previous one, except for some slight differences in the loop pressure (51 bars) and power supplied by heaters (39 and 21 kW).

4ST24-06-98 – The test was conducted with the same loop configurations of the previous tests except for the status of the main valve FT213 that was partially closed (70%). The compressor still operating at 13000 rpm supplied a lower mass flowrate (0,173 kg/s) and consequently a lower power was supplied by the heaters (31 and 16 kW).

5ST24-06-98 – This test was carried out at higher helium temperature than the previous ones and 51 bar pressure. The compressor operated at 13000 rpm and provided 0,222 kg/s helium mass flowrate. The electrical power was supplied by heater E219/3 (26 kW) and by the 7-pin TS (71 kW). The control of the regulation valves FT 213, FT234, FT235 was not active. The

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main valve FT213 was completely open, whereas the by-pass valve FT234 and FT235 were closed.

6ST24-06-98 – This test was carried out at the same configurations and conditions as the previous one. A higher electrical power supplied only by the 7-pin Test Section (118 kW) led the helium in the hot zone of the loop to higher temperatures.

7ST25-06-98 – This test was carried out at 51 bar pressure and at about the same helium temperature of the previous one but with a different loop configuration. The compressor supplied 0.227 kg/s mass flowrate at 13000 rpm. The electrical power was supplied only by the 7-pin test section (130 kW). The hot by-pass valve FT 234 was controlled in order to guarantee 300 °C helium temperature at the inlet of the TS. Owing to this control the valve resulted partially open (37%), while the main valve FT 213 was maintained completely open.

8ST25-06-98 and 9ST25-06-98 – These tests were conducted at the same conditions and loop configuration as the previous one.

40%ST19-02-99 – This test was carried out at relatively low helium pressure (23 bars) and high temperature. The compressor supplied the facility with 0.1 kg/s helium mass flowrate at 14200 rpm to provide a quite high helium mass flowrate (0,222 kg/s). The electrical power was supplied by the 7-pin TS (94 kW). The hot by-pass valve FT 234 was controlled in order to guarantee 350 °C helium temperature at the inlet of the TS. Owing to this control the valve resulted partially open (47.7 %), the main valve FT 213 was partially open (88%) as well.

30%ST19-02-99 – This test was carried out at the same configurations and conditions as the previous one. The electrical power was supplied both by the Test Section (68 kW) and by the two heaters E219/3 (4 kW) and E219/2 (7 kW).

3.1.2 Experimental Data Description

The status of the loop is described through a series of 45 measurements that are provided for each steady state above described. The measurement series reported in Tab. 14 have been drawn from the original material recovered. For 6 steady states (1ST24-06-98, 2ST24-06-98, 7ST25-06-98, 8ST25-06-98, 40%ST19-02-99) they represent the average values on the last 10 minutes of a longer acquisition time; for 3 of them (4ST24-06-98, 5ST24-06-98, 9ST25-06-98) they are the average values on the only 10 minutes available. Finally for the 30%ST19-02-99 steady state only a synoptic with an instantaneous status of the loop is available.

The description of these 45 measurements is given in the following:

TR 218 – Economizer Outlet Temperature (Hot Side) [°C]
 TR 215 – Economizer Inlet Temperature (Cold Side) [°C]
 TR 217 – Economizer Inlet Temperature (Hot Side) [°C]
 TR 216 – Economizer Outlet Temperature (Cold Side) [°C]
 FIC 228X – Economizer Outlet Mass Flowrate (Hot Side) [kg/h]
 TR 239 – Cold Mixer Outlet Temperature [°C]

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TIC 242X – Air Cooler Outlet Temperature (Helium) [°C]
 TR 267 - Air Cooler Inlet Temperature (Air) [°C]
 TR 266 - Air Cooler Outlet Temperature (Air) [°C]
 TR 242W - Air Cooler Outlet Temperature (Helium) for Fan Regulation [°C]
 TR 202 - Compressor Inlet Temperature [°C]
 TR 204 - Compressor Outlet Temperature [°C]
 PDR 201 – In-Out Compressor Differential Pressure [bar]
 FIC 212W – Helium Mass Flowrate for Compressor Control [kg/h]
 FIC212X - Compressor Outlet Mass Flowrate [kg/h]
 FIC228W – Mass Flowrate Set Point for Regulation of Valves V235 [kg/h]
 FIC228Y – Signal for Regulation of Valves V235 (%)
 ZR 235 – Opening of Valve V235 (%)
 ZR 213 – Opening of Valve V213 (%)
 ZR 234 – Opening of Valve V234 (%)
 TR 220 – Heater E219/3 Inlet Temperature [°C]
 TR 221 – Heater E219/3 Outlet Temperature [°C]
 TR 226 – Heater E219/3 Rod Temperature [°C]
 TIC 222X - Heater E219/2 Outlet Temperature for Power Regulation [°C]
 TIC 222W - Heater E219/2 Outlet Temperature Set Point for Power Regulation [°C]
 TIC 222Y – Signal for Regulation of E219/2 Electrical Power [%]
 TR 225 – Heater E219/2 Rod Temperature [°C]
 TIC 223X - Heater E219/1 Outlet Temperature for Power Regulation [°C]
 TIC 223W - Heater E219/1 Outlet Temperature Set Point for Power Regulation [°C]
 TIC 223Y – Signal for Regulation of E219/1 Electrical Power [%]
 TR 224 – Heater E219/1 Rod Temperature [°C]
 TIC 232X – Test Section Inlet Temperature for Regulation Valves V234/V213 [°C]
 TIC 232W –Set Point for Regulation Valves V234/V213 [°C]
 TR 233 - Test Section Outlet Temperature [°C]
 TR 241 - Compressor Inlet Temperature for Protection System [°C]
 TR 236 - Heater E219/1 Inlet Temperature for Protection System [°C]
 TR 297 - Heater E219/2 Inlet Temperature for Protection System [°C]
 TIC 242Y – Signal for Regulation Fan [%]
 TIC 232Y – Signal for Regulation Valves V234/V213 [%]
 ST 270 – Compressor Speed [rpm 10⁻²]
 PR 298 – Compressor Inlet Pressure [bar]
 PR 206 – Tank Pressure [bar]
 PR 227 – Test Section Inlet Pressure [bar]
 PDR 229 – In-Out Test Section Differential Pressure [bar]
 FIC 212Y – Signal for Compressor regulation

3.1.3 Experimental Data Evaluation

The acquisition of the measured parameters above described was not followed by a qualification to associate the uncertainty range to the experimental data. The accuracy of the most part of the instrumentation was declared to be within the range of 0.5 % of the instantaneous value. For the temperature measurements that should be equivalent to an uncertainty of $\pm 2\text{-}3$ °C in the hot side of the loop and ± 1 °C in the cold one. Unfortunately no

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information is available about the real status of the instrumentations during the tests. It is worth to highlight that the few observations in the following have been deduced from an analysis of the experimental data performed about 8 years later.

The distribution of temperature along the loop should be completely characterized through 17 thermocouples properly located. The reliability of the measured values is for a few of them rather questionable. In particular, the temperature TR233 located at the Test Section outlet is completely unreliable, as the recorded values are about 100 °C more than expected with an energy balance on the TS. Moreover, the tests with the TS at 0-power (1/2/4ST24-06-98) show clearly a constant over prediction (8°C) of the temperature at the inlet of the economizer hot side (TR307) that seems to affect all the tests. Some loop positions are provided with two or more instruments that should give very close temperatures. In two cases this is not the reality; in fact, at the economizer cold side outlet TR216 and TR220 differ of about 10 °C as well as at the economizer hot side outlet, where TR218 and TR217 differ of 8-10 °C. According to the notes taken by the operators during the tests, the thermocouple at the compressor outlet (TR204) recorded a value of a few degrees °C (2-3) higher than the value displayed on the compressor console that was considered more reliable.

The compressor speed measurement (ST 270) is not reliable at all. According to the operators the signal to be used for the compressor speed evaluation is FIC 212Y that represents the ratio of the instantaneous speed respect to the maximum speed (18000 rpm). For instance, the value of 0.72 recorded in almost all tests corresponds to 13000 rpm.

Because no information is available about the installation of the thermocouples on the heaters roads (TR224/5/6), a particular caution is recommended in using them. During the steady state tests the signals related to the thermocouples installed in the TS pins were not acquired.

The two mass flowrate measurements at the economizer outlet (FIC 228X) and at the compressor outlet (FIC 212X) generally differ less than 1,5 %, in very good agreement with the accuracy of the instruments ($\pm 0.5\%$), thus partially confirming the low values declared for the helium leakage in the loop.

The pressure drops of the loop are not completely characterized. Only two accurate measurements ($\pm 0.5\%$) are installed through relevant parts of the loop as the compressor (PDR 201) and Test Section (PDR 229). The pressure signals are not sufficiently accurate to be used for it (± 1 bar).

There is no signal related to the amount of electrical power supplied in the test section. The information, which has been reported in the test descriptions, has been deduced from the notes taken by the operators during the tests and verified by means of an energy balance on the Test Section.

An energy balance on the whole loop has been calculated for some tests in order to provide an estimate of the thermal losses. The results of these calculations are collected in Tab.14. It has to be observed the large spread of the values that depends by several reasons:

- the different conditions of the tests, the heat losses depends on the helium temperature both in term of temperature drops and for the increase of the rock wool conductivity with the temperature;
- the uncertainty on the helium temperatures used for the balances, which is estimated to account for an uncertainty of ± 5 kW on the total heat losses;
- the presence of important thermal bridges in large components like the heaters and the economizer;
- for some tests the limited period of acquisition documented can give rise to some doubts on the effect of the relatively high thermal capacity of the structural material (walls, rods).

Steady State Test	Loop Heat Losses (W)
2ST24-06-98	4800.
4ST24-06-98	5200.
5ST24-06-98	23000.
6ST24-06-98	31000
7ST24-06-98	21900.

Tab.14 – Estimated Thermal Losses in Steady State Tests

3.2 Transient Tests

Two transient tests simulating loss of flow events in the test section were conducted in the HE-FUS3 facility on 9th of July 1998. They are identified with a two digit number (50 and 30) that refers to the power in % supplied by the Test Section, followed by LOFA to indicate the kind of transient and by the indication of the day (e.g. 50LOFA09-07-98).

3.2.1 Facility Configurations

In the following for each test will be described the status of the loop in term of initial and boundary conditions and the status of the controls: pressure, mass flowrate, electrical power and way to supply it, active controls description.

50LOFA09-07-98 – The test was carried out at about 50 bar pressure and at quite high temperature (400 °C at test section outlet). The compressor operating at 13000 rpm supplied 0,216 kg/s helium mass flowrate. The electrical power was supplied only by the 7-pin test section (118 kW) manually settled. The hot by-pass valve FT 234 was controlled in order to guarantee 300 °C helium temperature at the inlet of the TS. Owing to this control the valve resulted slightly open (17%), while the main valve FT 213 was maintained completely open. The cold by-pass valve FT235 was closed at the beginning of the test.

After reaching the initial steady state the cold by-pass valve FT 235 was opened in about 10 s to simulate a sudden decrease of the flow rate in the test section (partial LOFA). The helium mass flowrate halved and consequently the TS rods temperatures and the helium TS outlet temperature increased. The modified conditions of cold and hot flows in the economizer affected the temperature at the cold side outlet that increased of about 15 °C. As a

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consequence the control system actuated a very slight opening of the valve FT 234 to maintain the TS inlet temperature at 300°C. The compressor control was inactive and the compressor speed remained constant (13000 rpm) during the transient. The compressor mass flow rate increased at the opening of the valve FV235 as a consequence of the different hydraulic characteristic of the loop.

The valve FV235 was closed after about 1 minute of transient in 6 s. Due to the high thermal inertial of the structural material and heated pins the helium temperature decreased very slowly.

The trends of the main parameters of the loop are reported in Figs. 20 to 23.

30LOFA09-07-98 – The test was carried out at about 50 bar pressure and at lower temperature than the previous transient (350 °C at test section outlet). The compressor operating at 13000 rpm supplied 0.217 kg/s helium mass flowrate. The electrical power was supplied both by the 7-pin test section (71 kW) manually settled and by the heater E219/1 (? kW) controlled by the corresponding helium outlet temperature with a set point of 300 °C. The main valve FT213 was completely open during the test, whereas the hot by-pass valve FT234 was closed. The cold by-pass valve FT235 was closed at the beginning of the test.

After reaching the initial steady state the cold by-pass valve FT 235 was opened in about 10 s to simulate a sudden decrease of the flow rate in the test section (partial LOFA). The helium mass flowrate halved and consequently the TS rods temperatures and the helium TS outlet temperature increased. The modified conditions of cold and hot flows in the economizer affected the temperature at the cold side outlet that increased of about 10 °C. As a consequence the control system switched off the heater E219/1 while no operation was made on valve FT213 and FT234. The compressor control was inactive and the compressor speed remained constant (13000 rpm) during the transient. The compressor mass flow rate increased at the opening of the valve FV235 as a consequence of the different hydraulic characteristic of the loop.

The valve FV235 was closed after about 150 s of transient in 6 s. Due to the high thermal inertial of the structural material and heated pins the helium temperature decreased very slowly.

The trends of the main parameters of the loop are reported in Figs. 24 to 27.

3.2.2 *Experimental Data Description*

The behavior of the loop during the transients is described through a series of 52 measurements. The 50LOFA09-07-98 series have been reported in Tab. B2 of the Appendix B as originally recovered, likewise the 30LOFA09-07-98 series are reported in Tab. B3. The acquisition frequency of the signals differed according to the type of measurement and its utilization. For instance, the helium temperatures were in general recorded every 16 s, while the signal used for the control system were recorded every 8 s.

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The file of the 50LOFA transient contains only 10 s of data recorded at the initial steady state conditions. Owing to the low acquisition frequency, most of the signals have only one value for the steady state characterization. The file of the 30LOFA transient contains 50 s at the initial steady state conditions, which allows defining the initial value of the parameters as an average among some data.

The first 45 signal recorded have been already described in the previous paragraph. The last 7 signals are related to the thermocouples implemented on the hot rods of the 7-pin Test Section (TT400, TT403, TT407, TT411, TT415, TT419, TT427). In Fig. 28 the location of these thermocouples is indicated.

3.2.3 *Experimental Data Evaluation*

The same remarks advanced for the steady state data in the previous paragraph are still valid for the parameters measured during the transient test. The energy balance at initial steady state conditions estimates a quite different amount of heat losses in the two tests: 25.6 kW in 50LOFA and 9 kW in 30LOFA. It seems very hard that the uncertainty on the temperatures and the different test conditions can completely explain such a large discrepancy. A further reason for it could be that the initial conditions for the 50LOFA transient were not completely stabilized. The registration available for this test starts about 10 minutes after the end of the registration of the previous 30LOFA test. Since in 30LOFA the hot part of the loop was at lower temperature the thermal capacity of the large components like economizer and heaters could have absorbed part of the power. This explanation is only a hypothesis because no experimental evidence is available.

3.3 Compressor Characterization Tests

Several experimental campaigns were carried out in February-March 1998 to characterize the prototypical generative compressor. The tests were conducted at different loop pressures varying the speed of the compressor and the hydraulic characteristic of the loop by means of the main valve F213 (see Fig. 18). The results reported in Tab. B4 and B5 respectively at 50 bar (COMP50-98) and 25 bar (COMP25-98) are related to the characteristics of the compressor as used for the steady states and transients carried out in 1998. As a new rotor was mounted at the beginning of 1999, the campaign was repeated at 25 bar (COMP25-99). These last data, which are the reference for the two steady states carried out in 1999, are reported in Tab. B6.

3.2.1 *Tests and data description*

The only information available about the configuration of the loop concerns the main valve that was used to change the hydraulic characteristic of the loop, thus obtaining several couples mass flowrate-head at constant speed. Anyway the temperature and pressure of the helium were maintained quasi-constant at the compressor inlet.

The series of data at different speeds (from 10000 rpm to 15000 rpm at 50 bar and from 10000 to 16000 at 25 bar) were obtained at 3-5 different position positions of the valve F213

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(the closing degree tested was more limited at high speed). Besides the loop parameter like inlet pressure, compressor differential pressure mass flowrate, inlet and outlet helium, also the parameter related the ancillary system for the electrical motor cooling (see Fig. 29) were recorded. As the auxiliary helium flow is derived at the compressor outlet and reintroduced at the compressor inlet, the mass flowrate and temperature are necessary for the correct mass and energy balances on the compressor.

In the following the description of the 7 measurements of the compressor tests is given:

FV10 - Compressor Speed [rpm]
 G 212 - Loop Mass Flowrate [kg/s]
 DP 201 - In-Out Compressor Differential Pressure [bar]
 Ti 202 - Compressor Inlet Temperature [°C]
 Pi 298 - Compressor Inlet Pressure [bar]
 Tout 204 - Compressor Outlet Temperature [°C]
 Tcusc 286 – Bearings Temperature [°C]
 Trit 275 – Auxiliary Loop Helium Return Temperature [°C]
 G 256 – Auxiliary Loop Helium Mass Flowrate [kg/s]

The auxiliary loop helium return temperature Trit 275 is available only for the COMP25-99 campaign. However its value is close to the bearings temperature Tcusc 286 that can be used to derive it.

Concerning the uncertainty on the experimental data the remarks advanced in the previous paragraphs are still valid both for the loop and ancillary system parameters.

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6. List of Figures

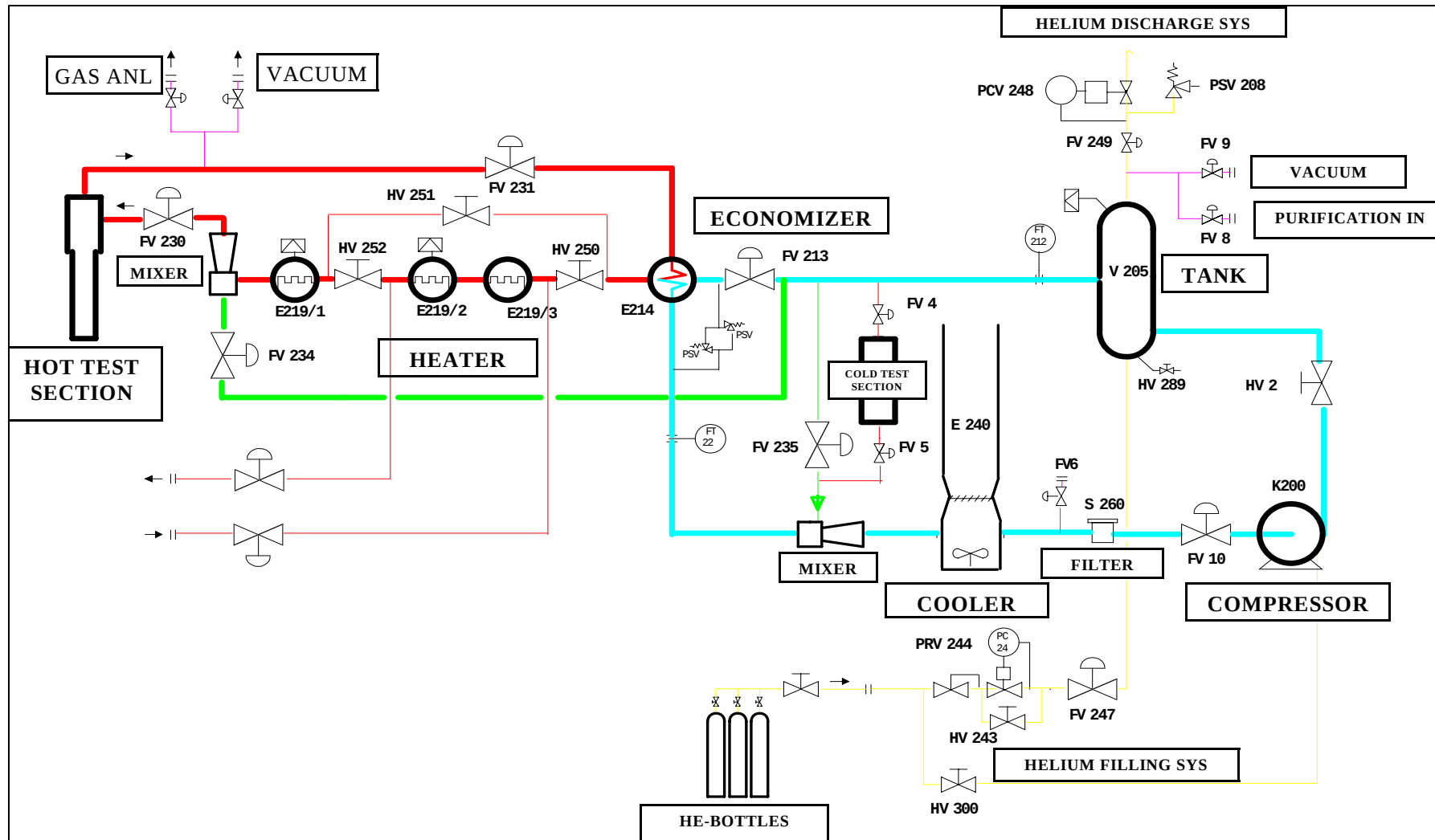


Fig. 1 – HE-FUS3 P&I Scheme

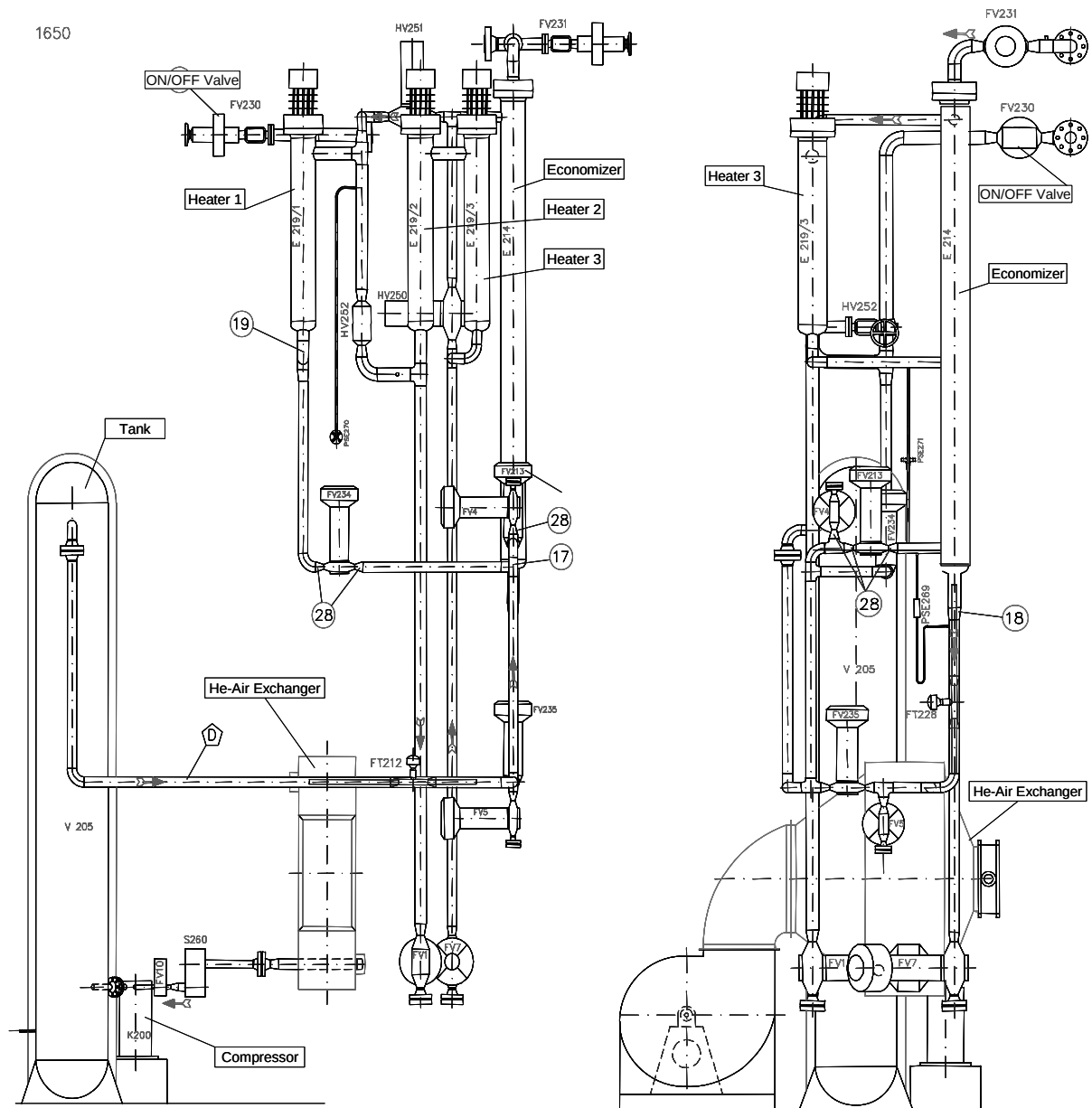


Fig. 2 – HE-FUS3 Vertical View

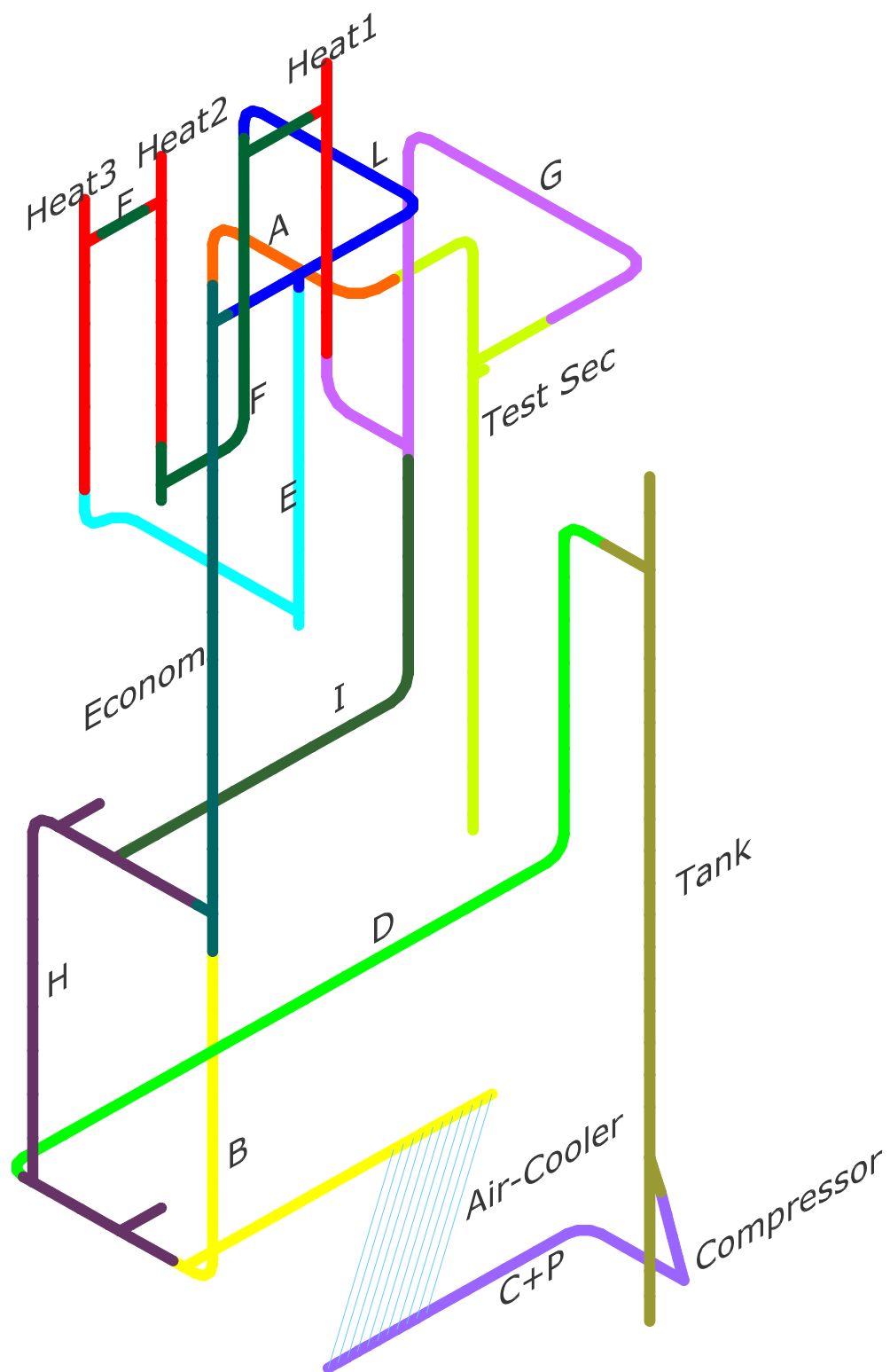


Fig. 3 – Piping Layout 3D Sketch

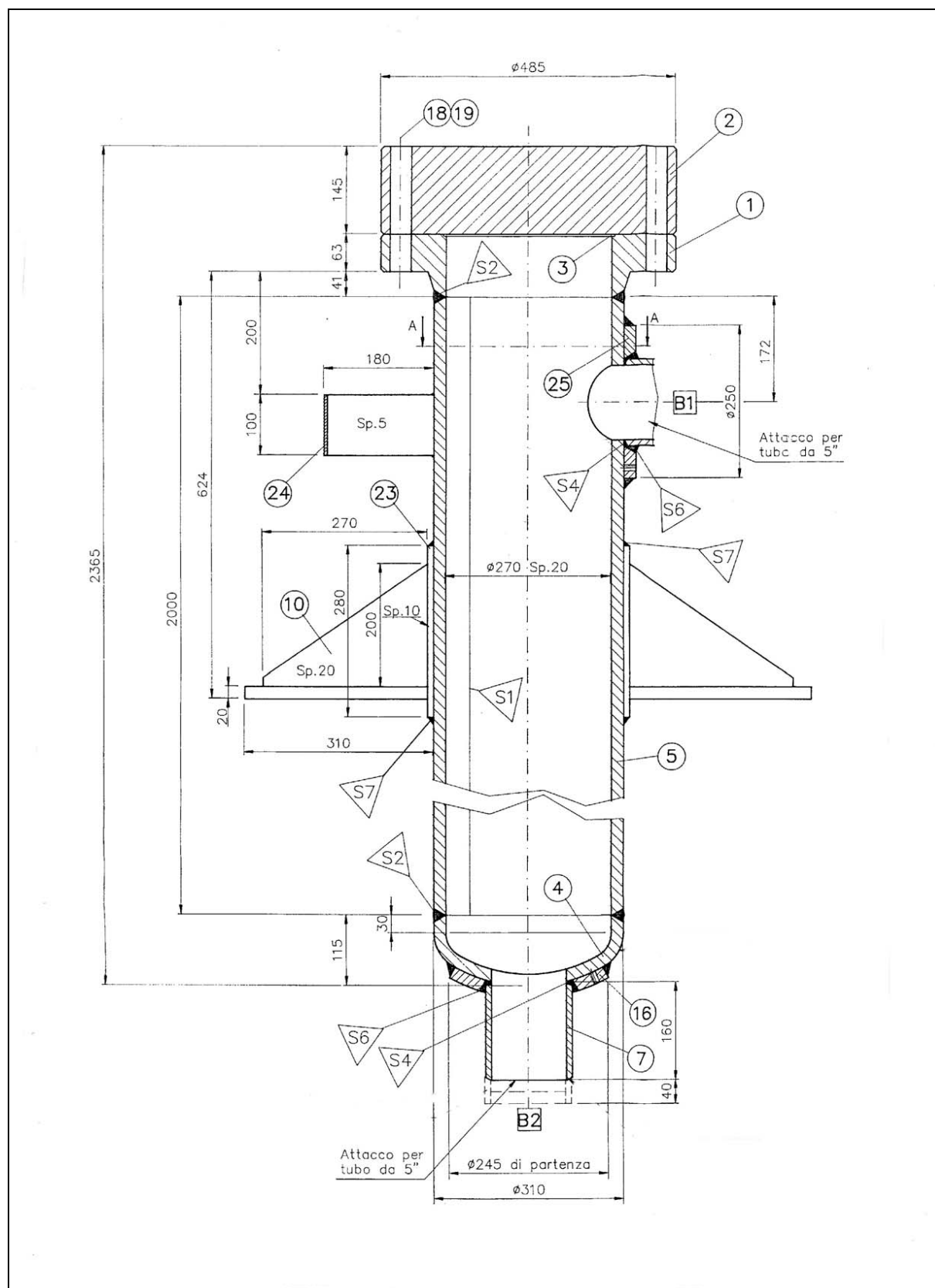


Fig. 4 – Electrical Heater Vessel

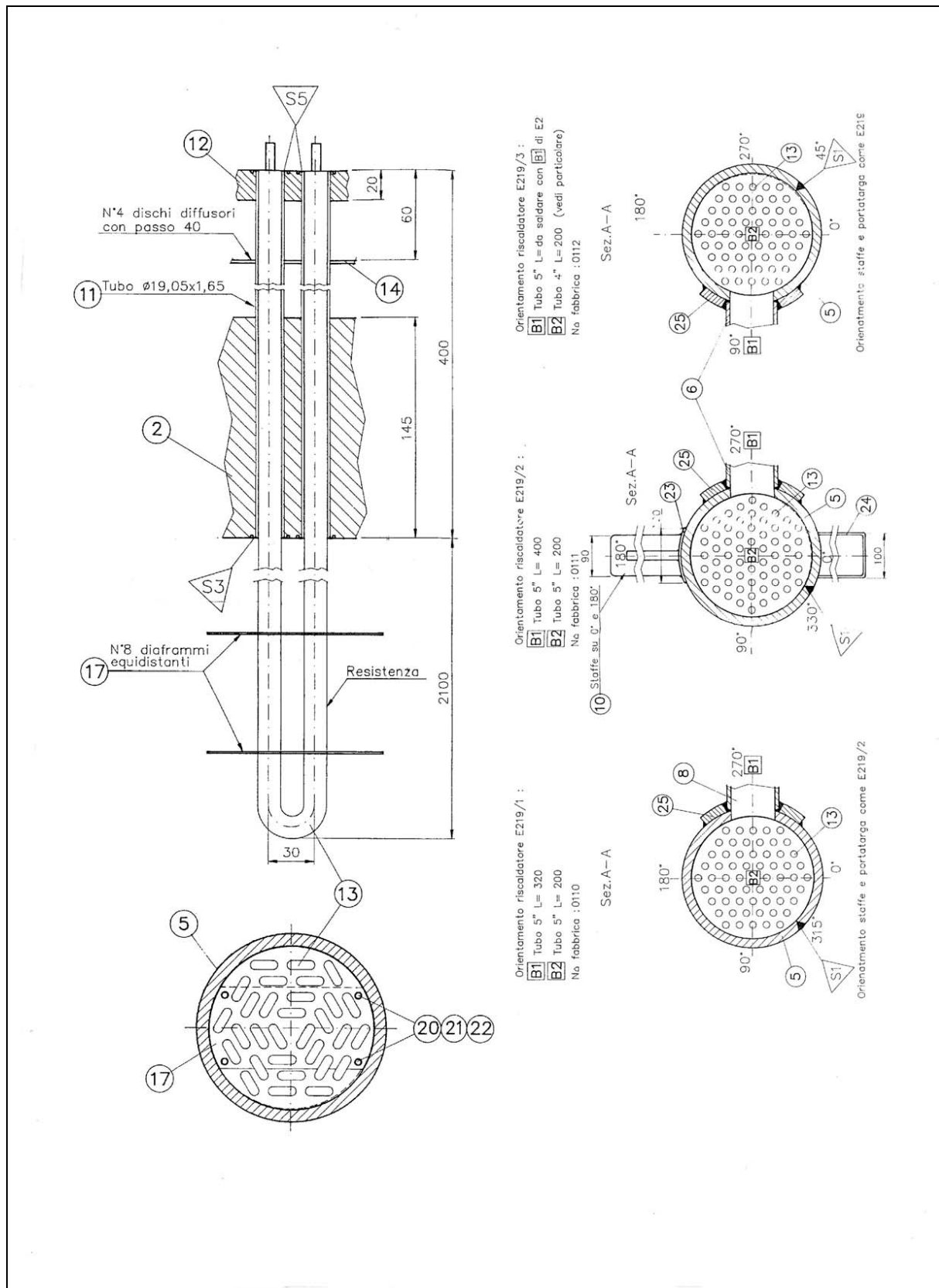


Fig. 5 – Electrical Heater Active Rods and Loop Connections

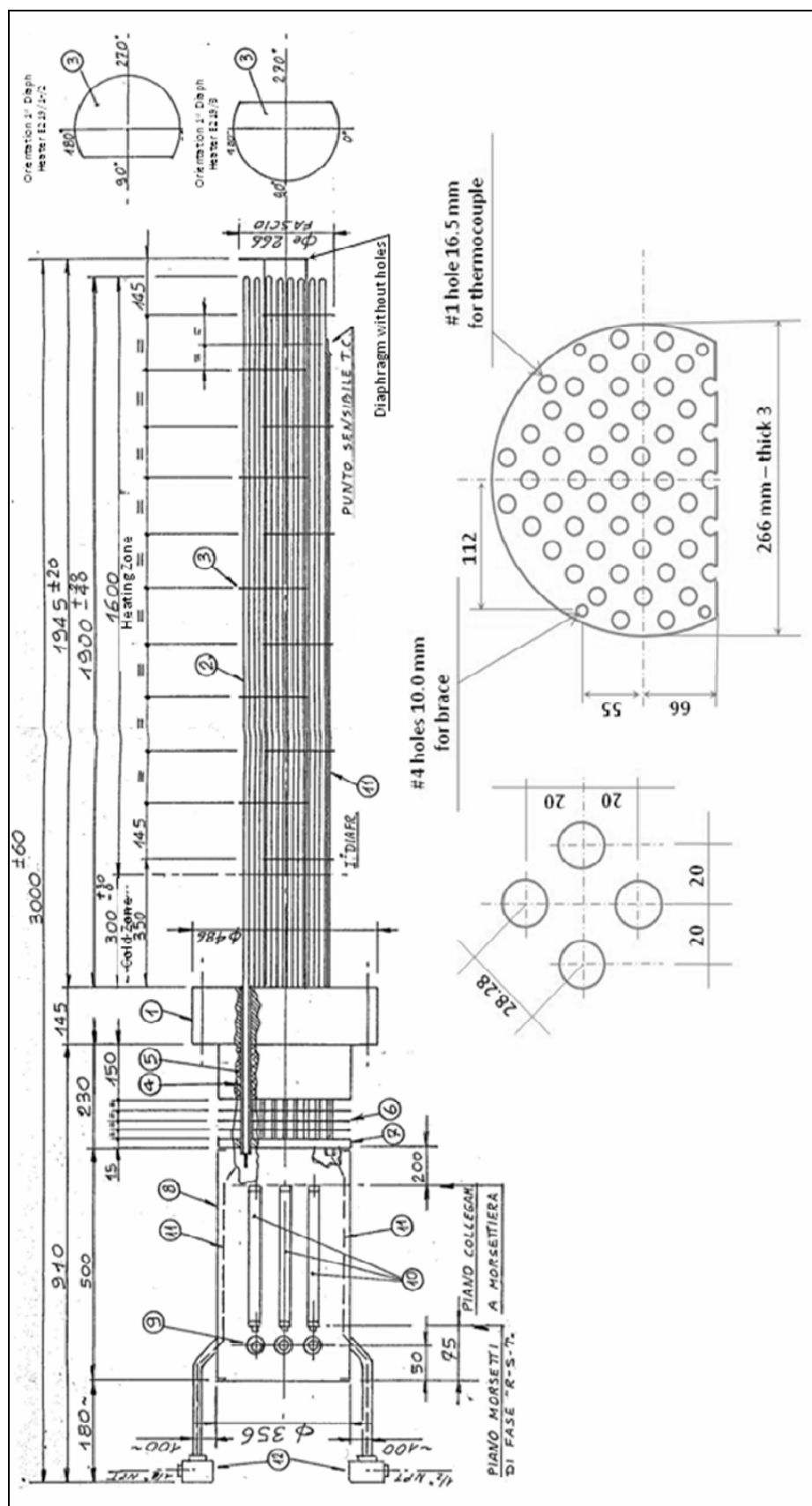


Fig. 6 – Electrical Heater Active Rods and Diaphragms Scheme.

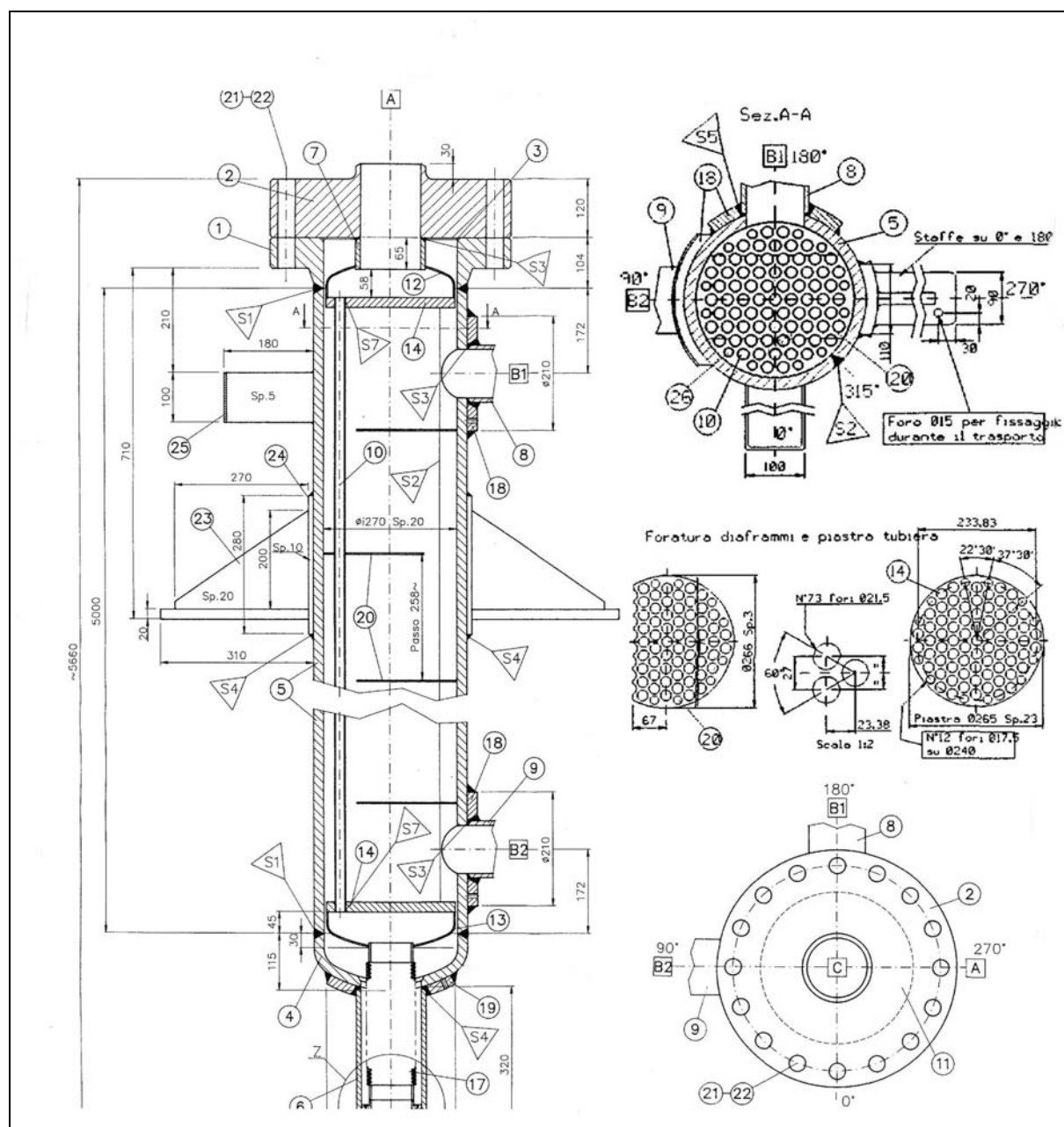


Fig. 7 – Economizer Vessel and Tubes Arrangement

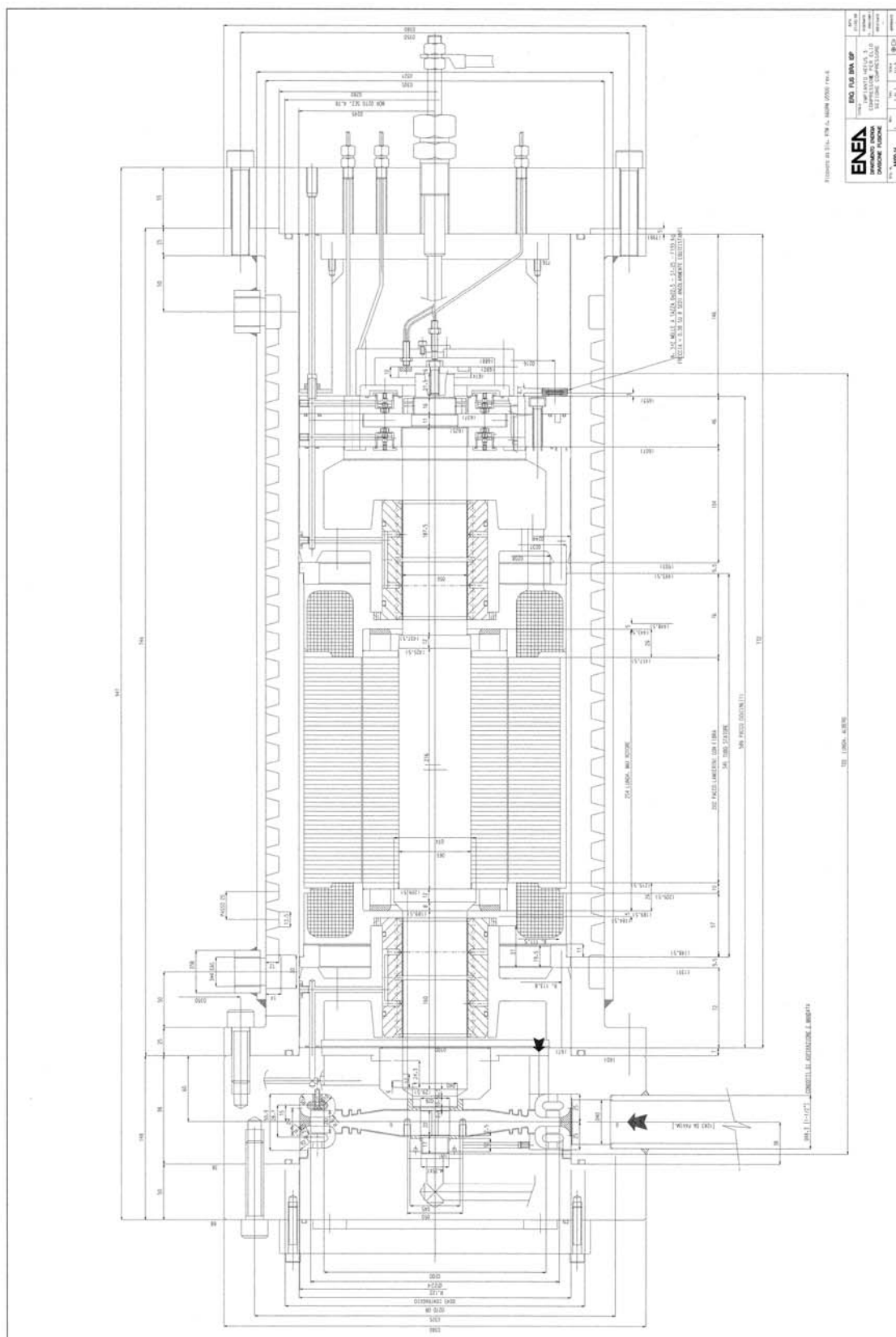


Fig. 8 – Regenerative Compressor

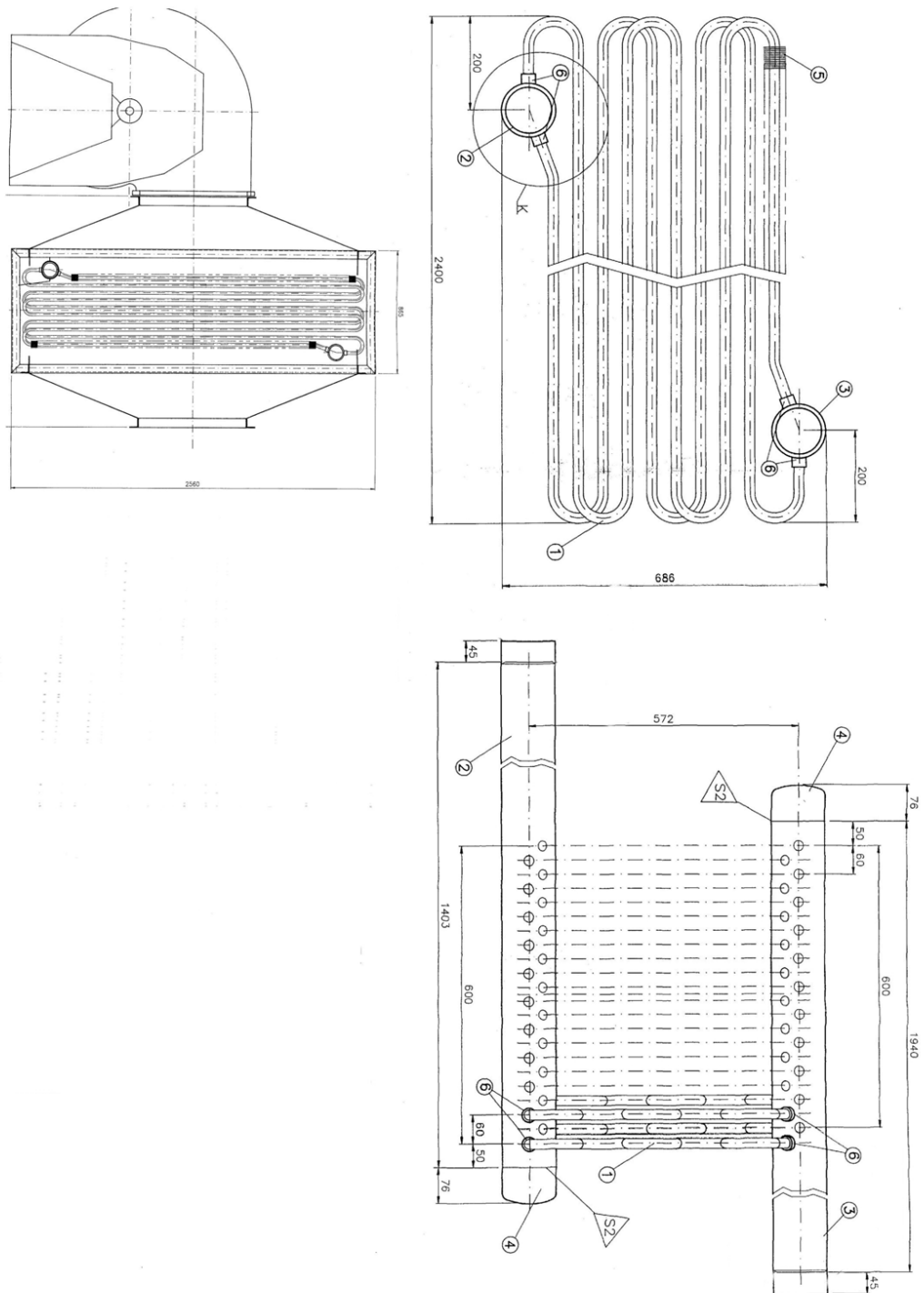


Fig. 9 – Air Cooler Case, Distributors and Finned Tubes

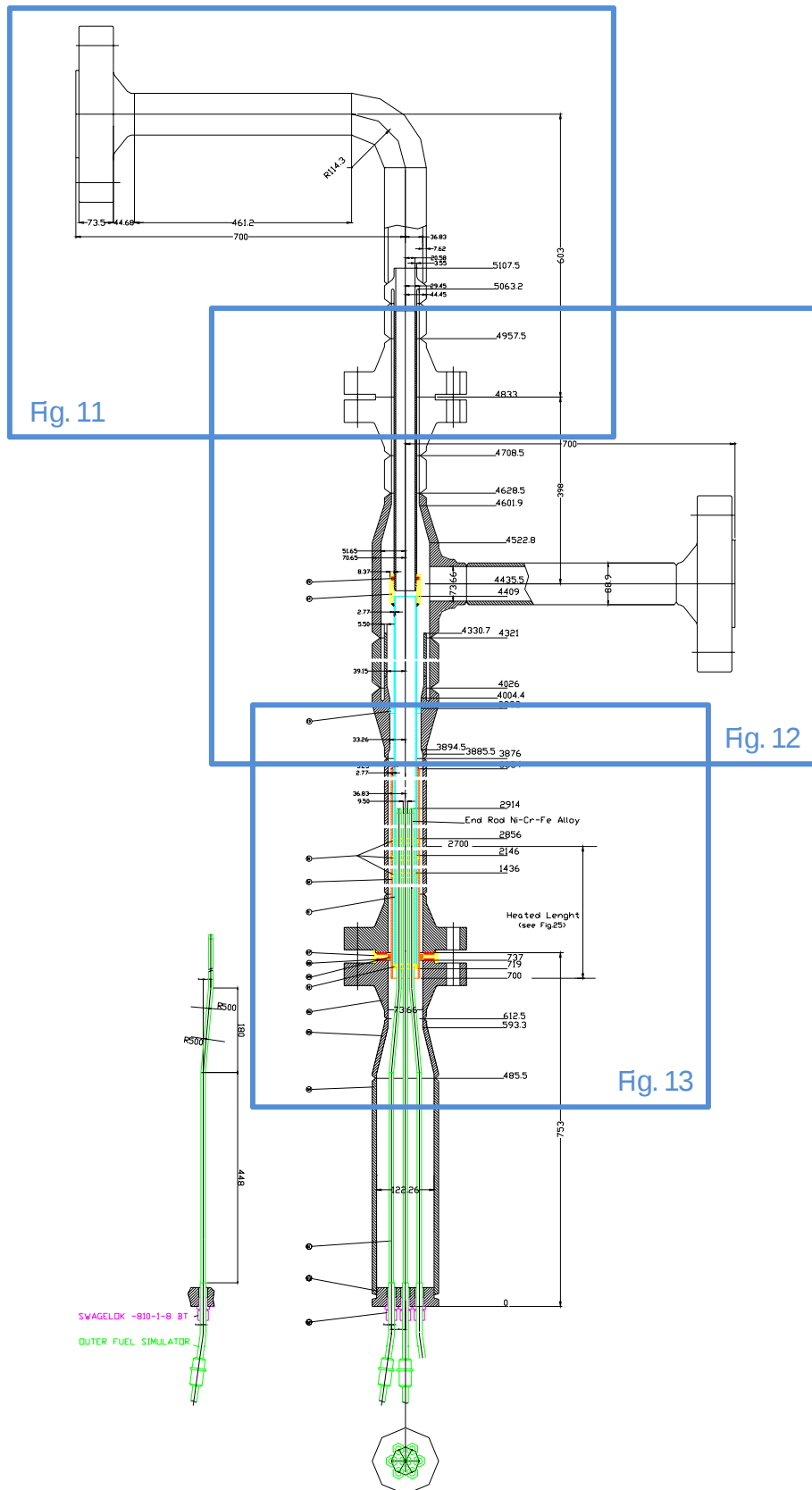


Fig. 10 – 7-pin Test Section Arrangement and Rod Grids

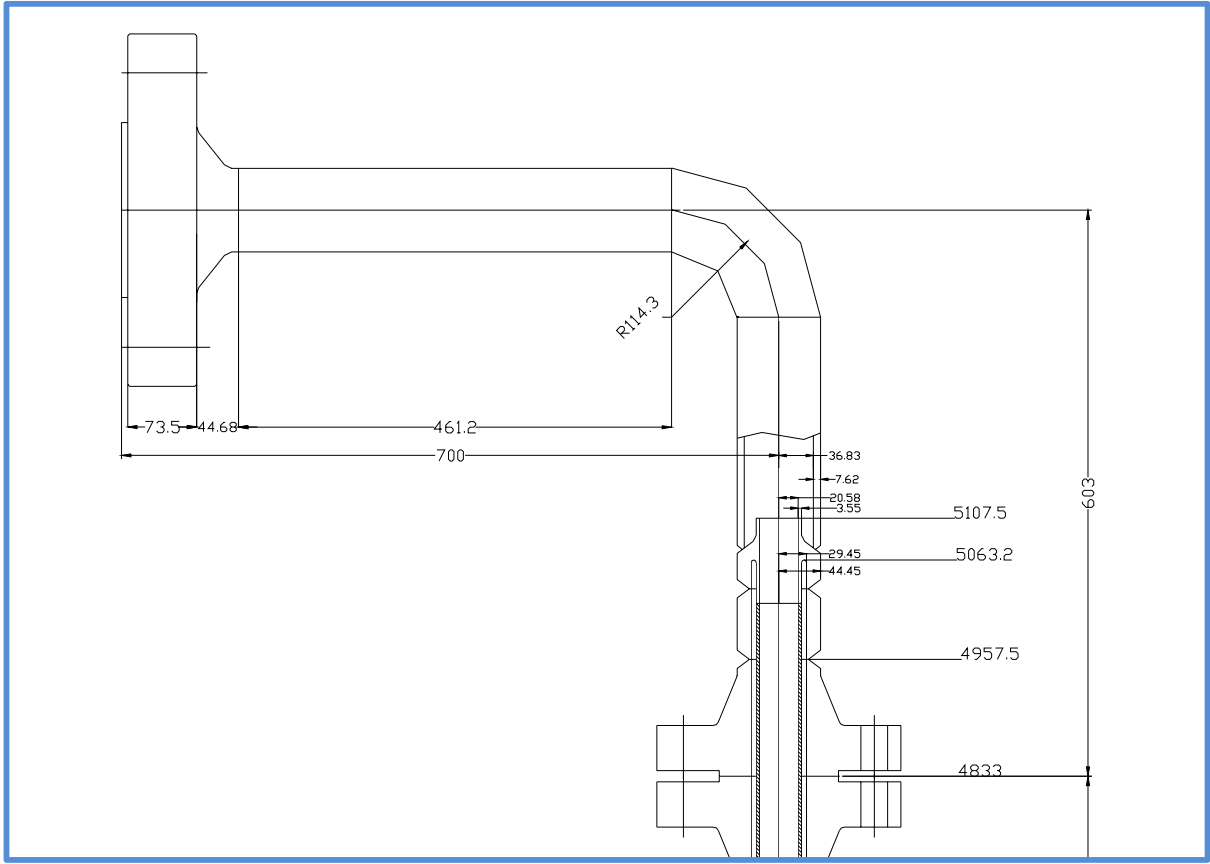


Fig. 11 – 7-pin Test Section – Upper Part

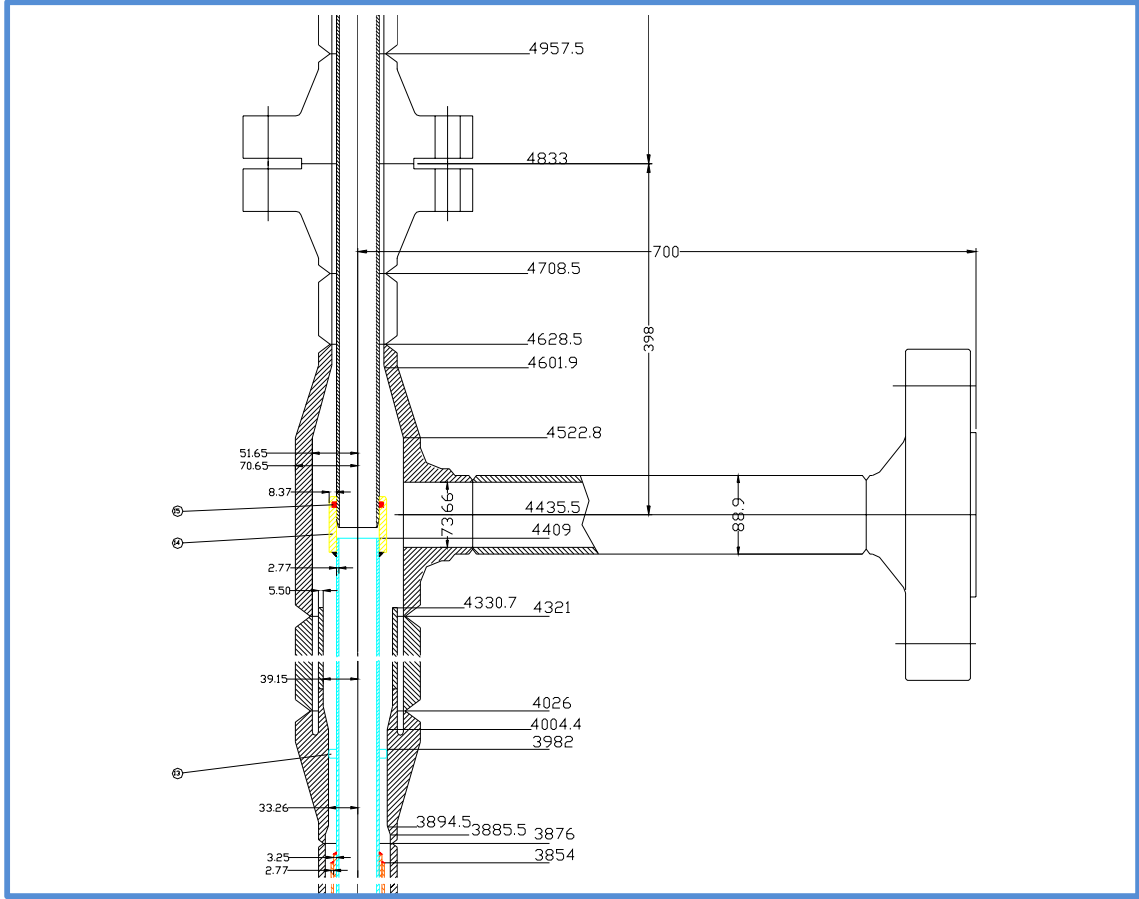


Fig. 12 – 7-pin Test Section – Intermediate Part

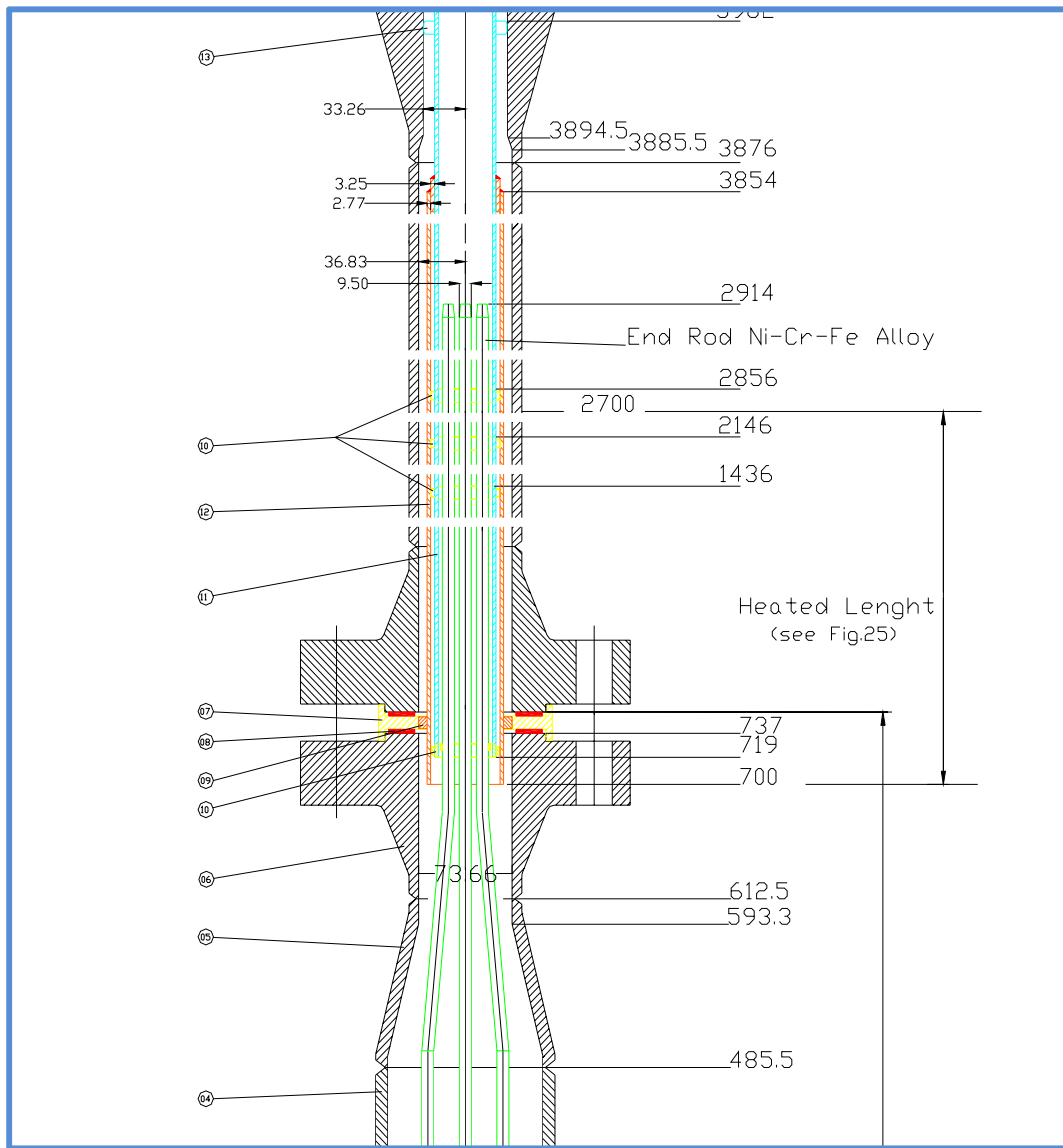
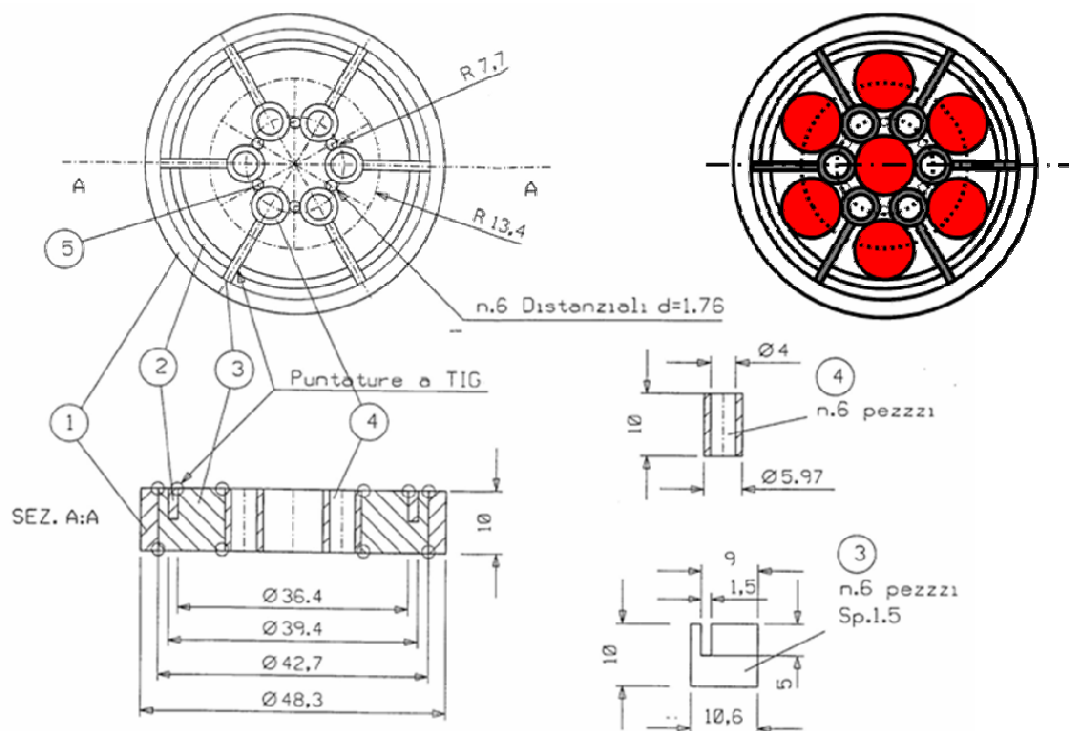


Fig. 13 – 7-pin Test Section – Lower Part



GRIGLIA DISTANZIATRICE (P/D=1.4105)

Fig. 14 – Test Section Grid and Rod Bundle (Pitch 29.6mm)

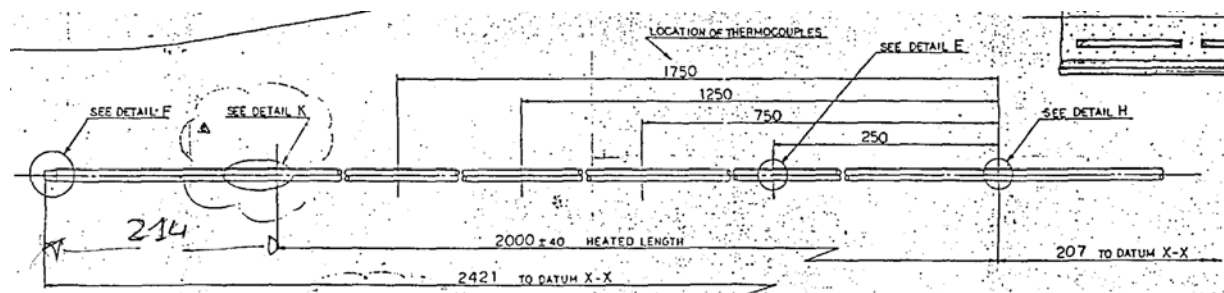


Fig. 15 – Particular of the Test Section Heating Rod with the position of the thermocouples

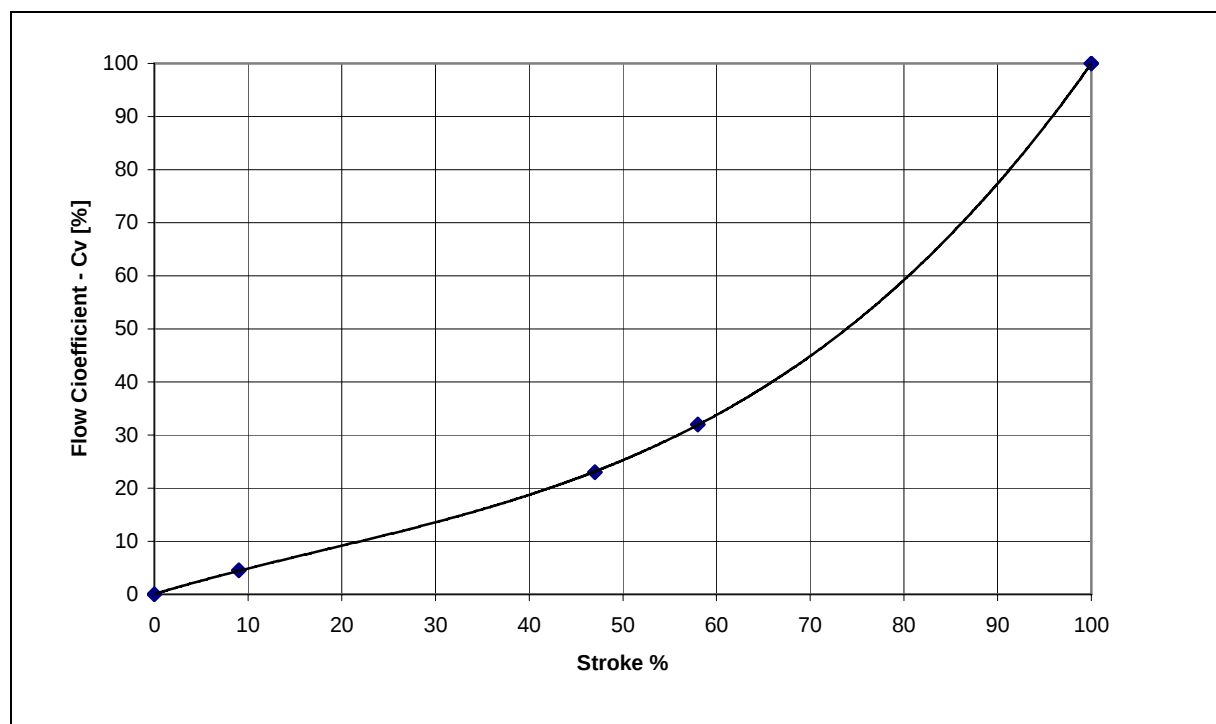


Fig. 16 – Characteristic of the Regulation Valves

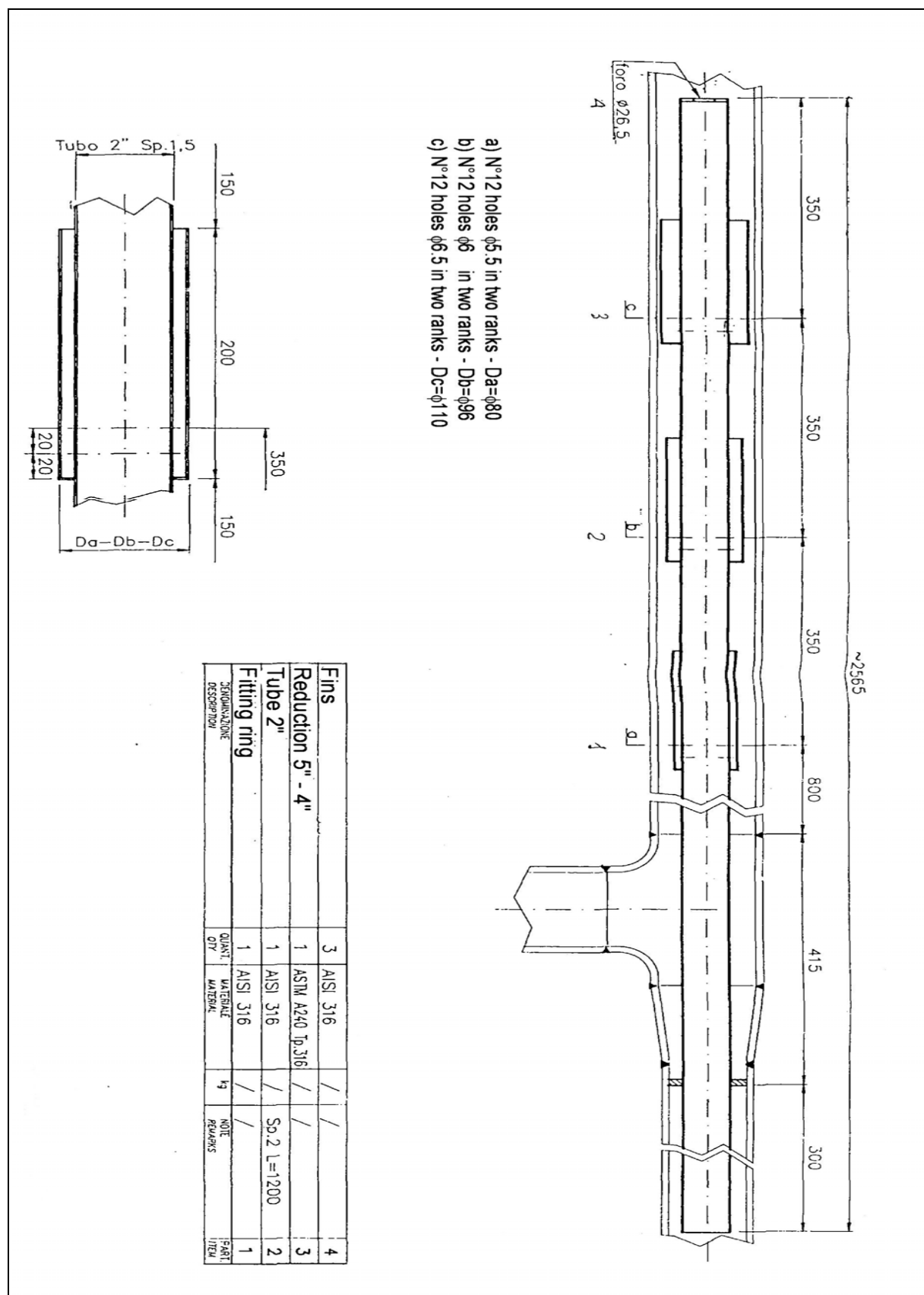


Fig. 17 – Single Module Mixer

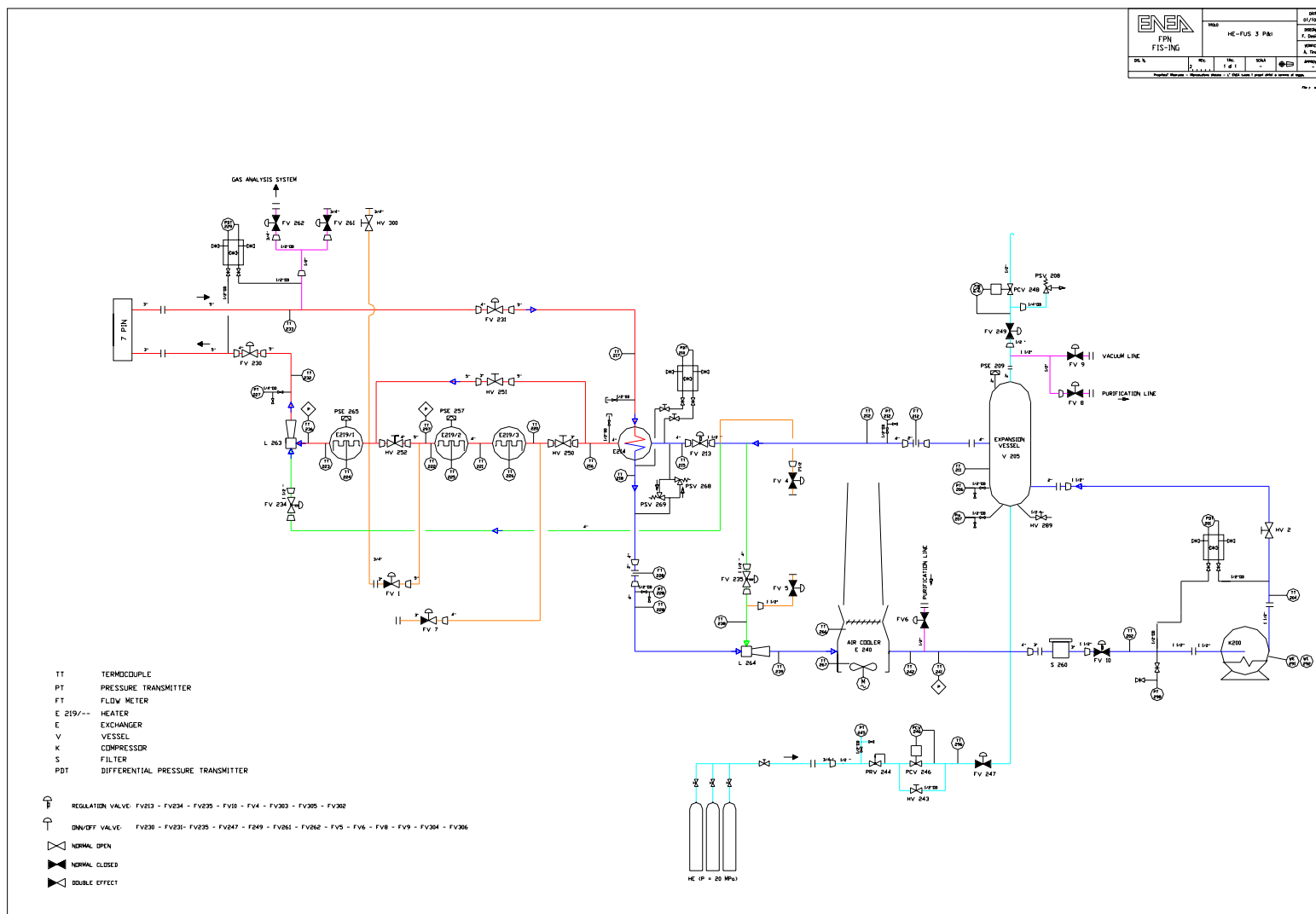


Fig. 18 – Instrumentation Map

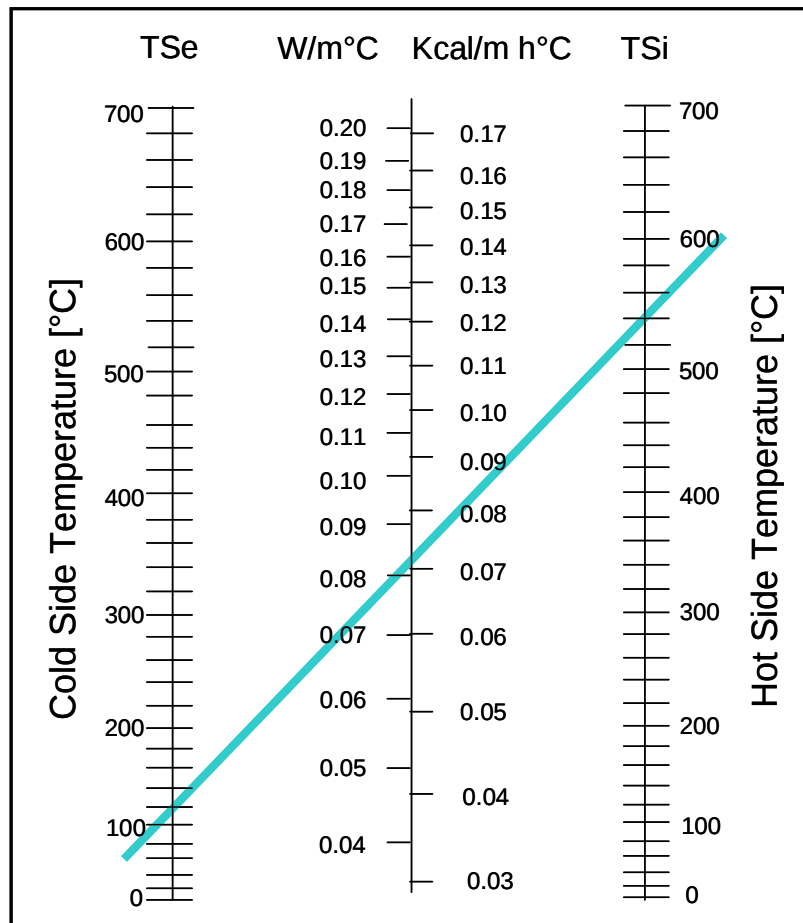


Fig. 19 – Thermal Conductivity of the Rock Wool

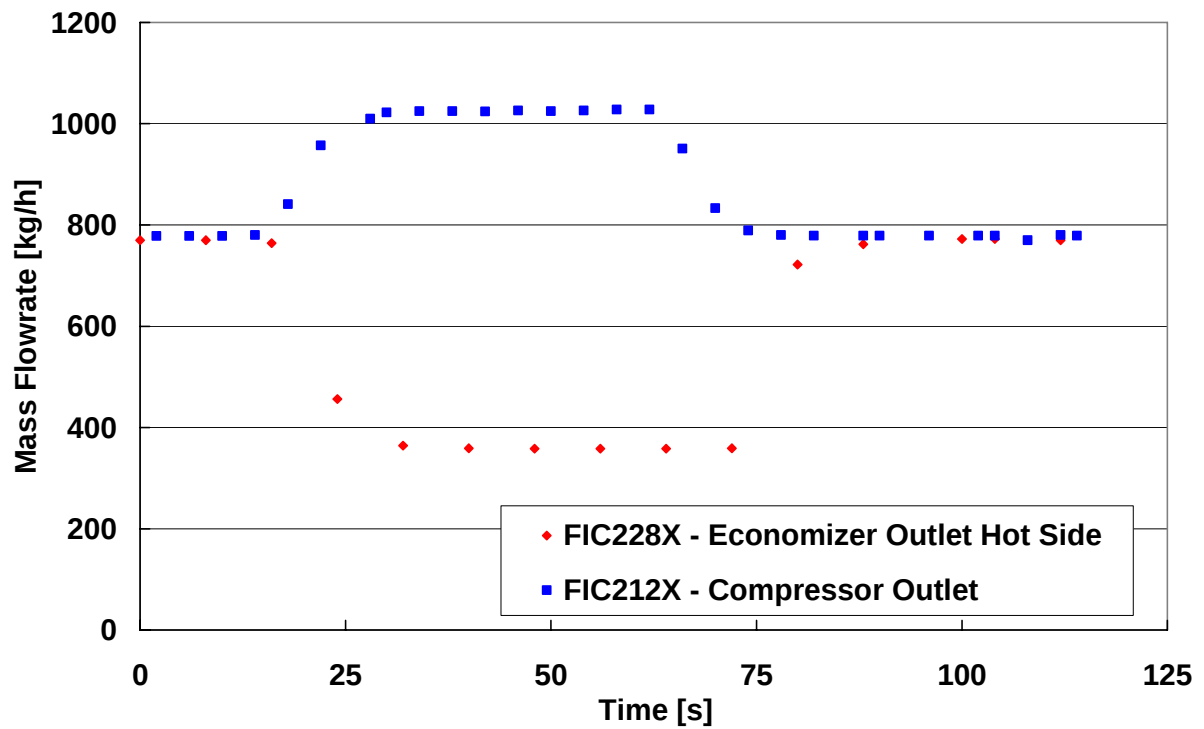


Fig. 20 – Test Section and Compressor Mass Flowrate (50LOFA09-07-98)

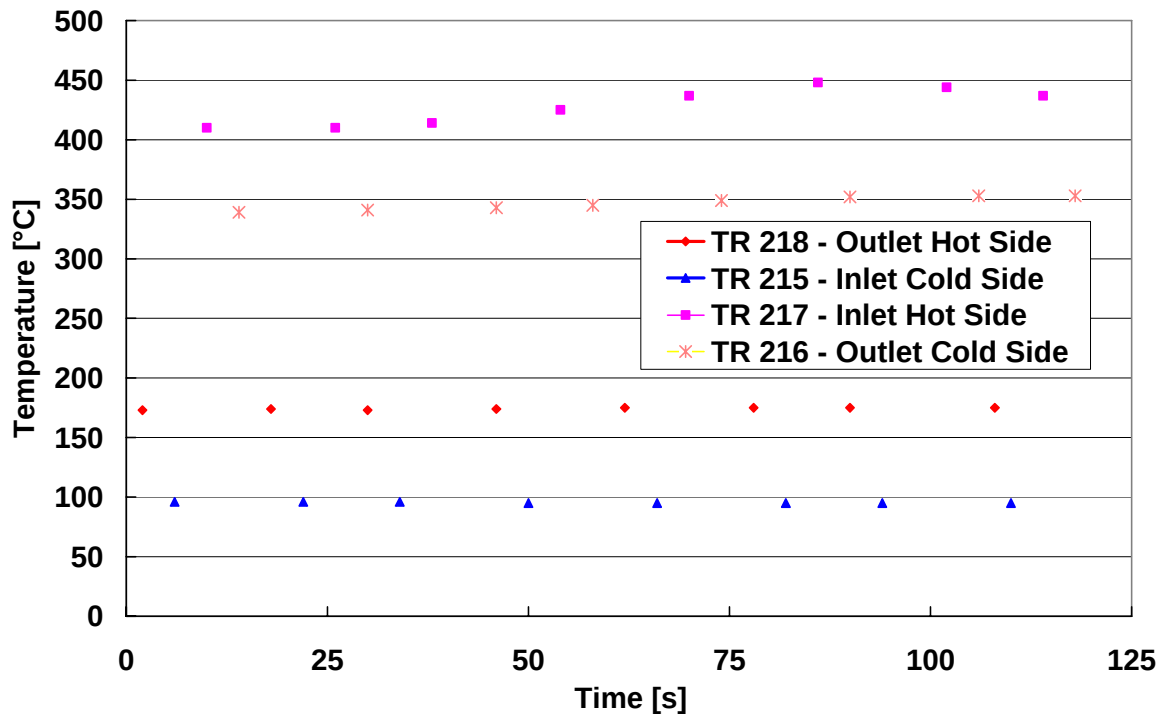


Fig. 21 – Economizer Temperatures (50LOFA09-07-98)

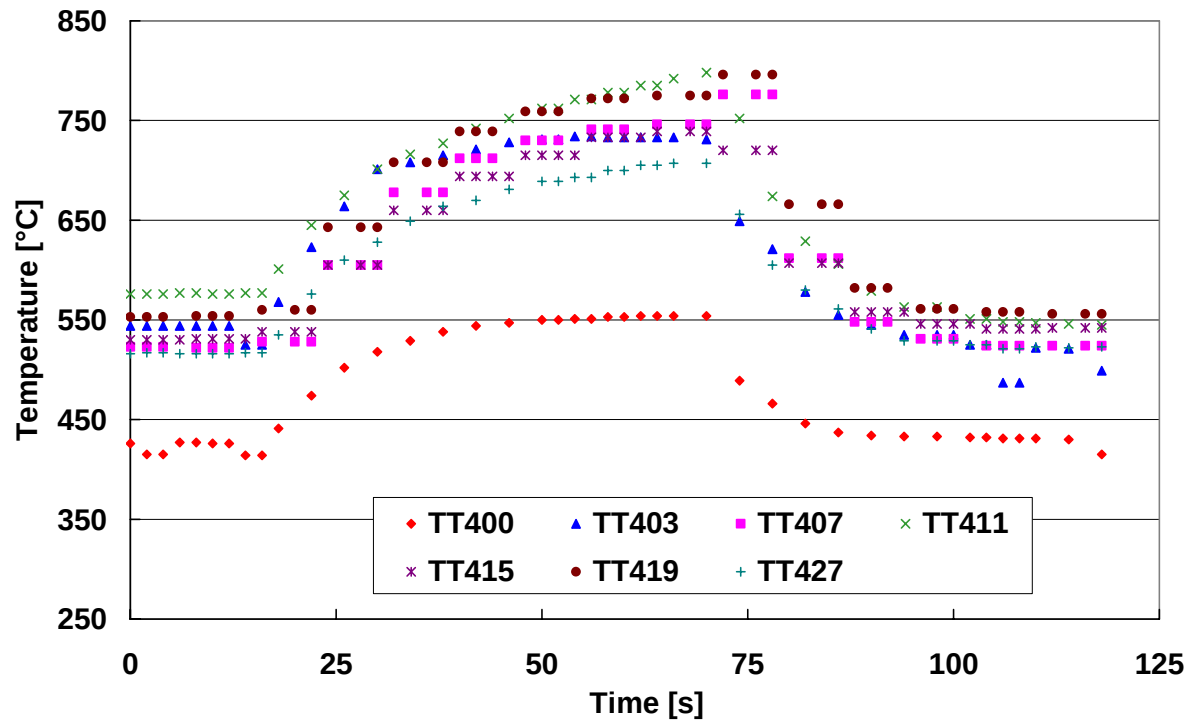


Fig. 22 – Thermocouple Temperatures on 7 TS Positions (50LOFA09-07-98)

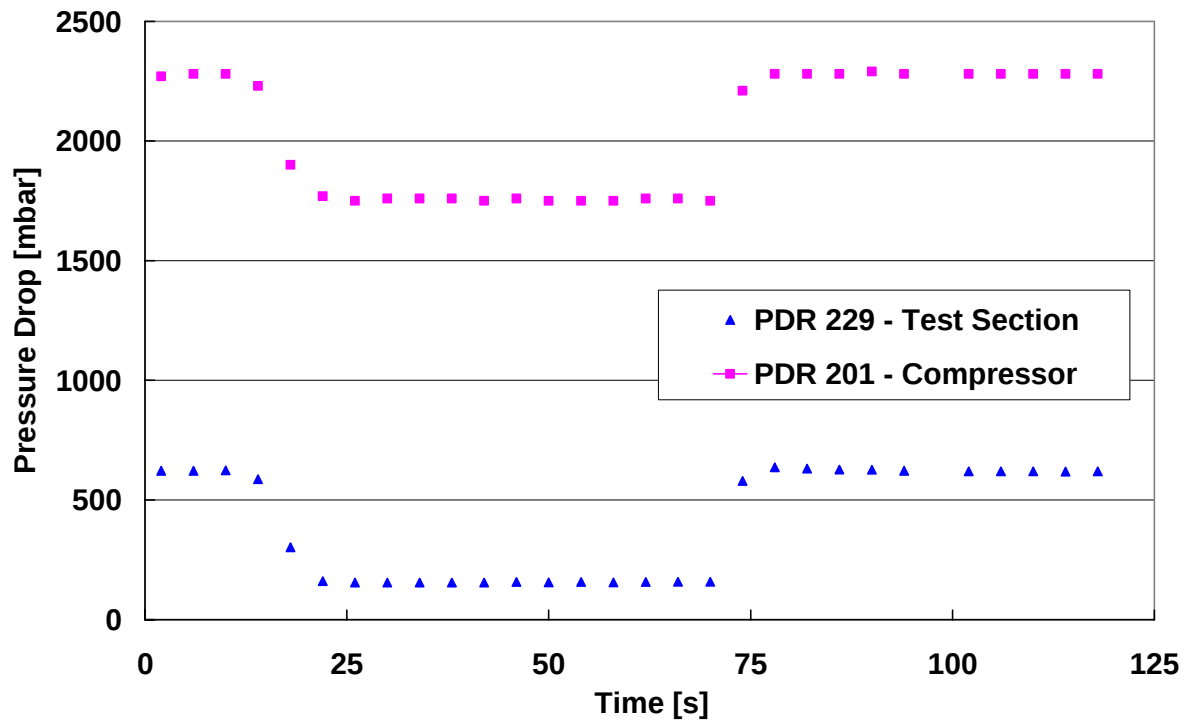


Fig. 23 – TS and Compressor Pressure Drop (50LOFA09-07-98)

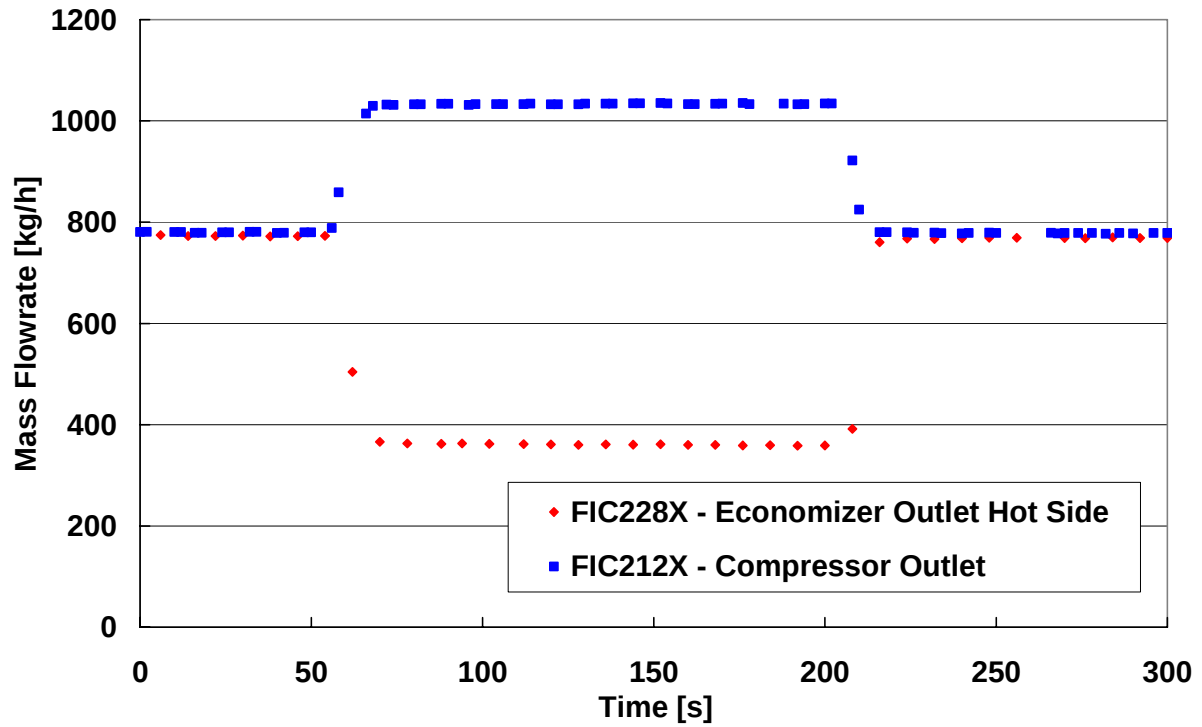


Fig. 24 – Test Section and Compressor Mass Flowrate (30LOFA09-07-98)

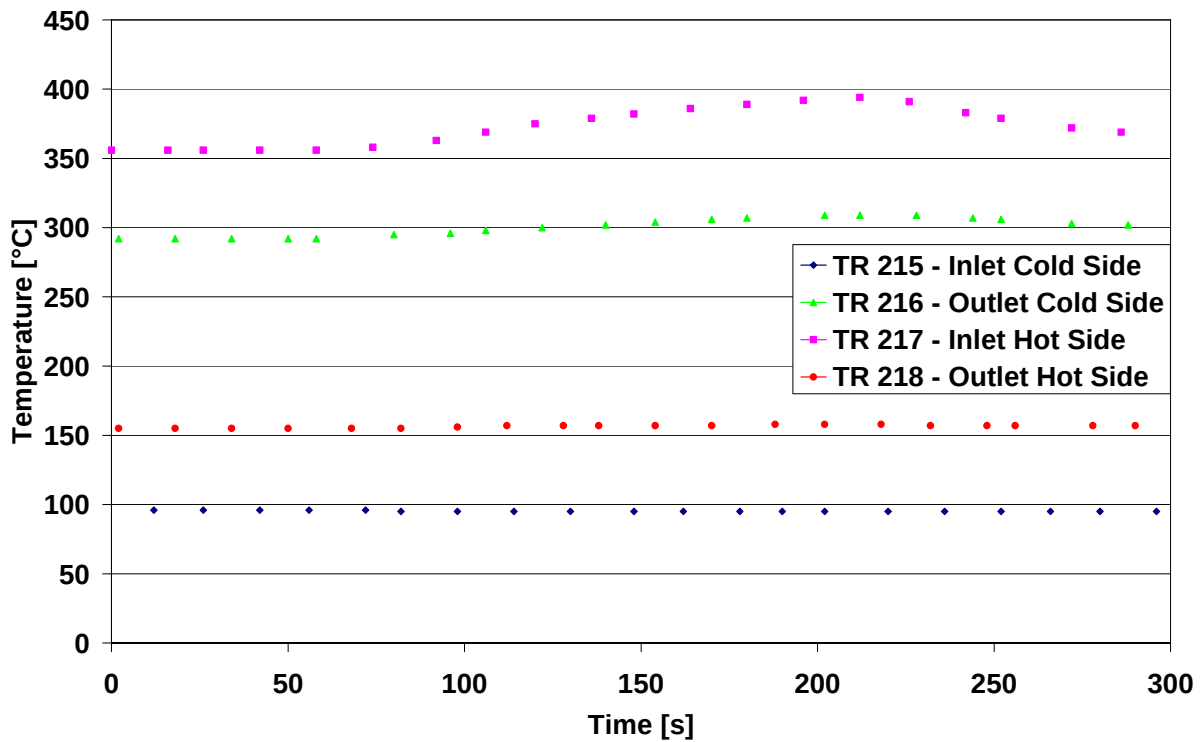


Fig. 25 – Economizer Temperatures (30LOFA09-07-98)

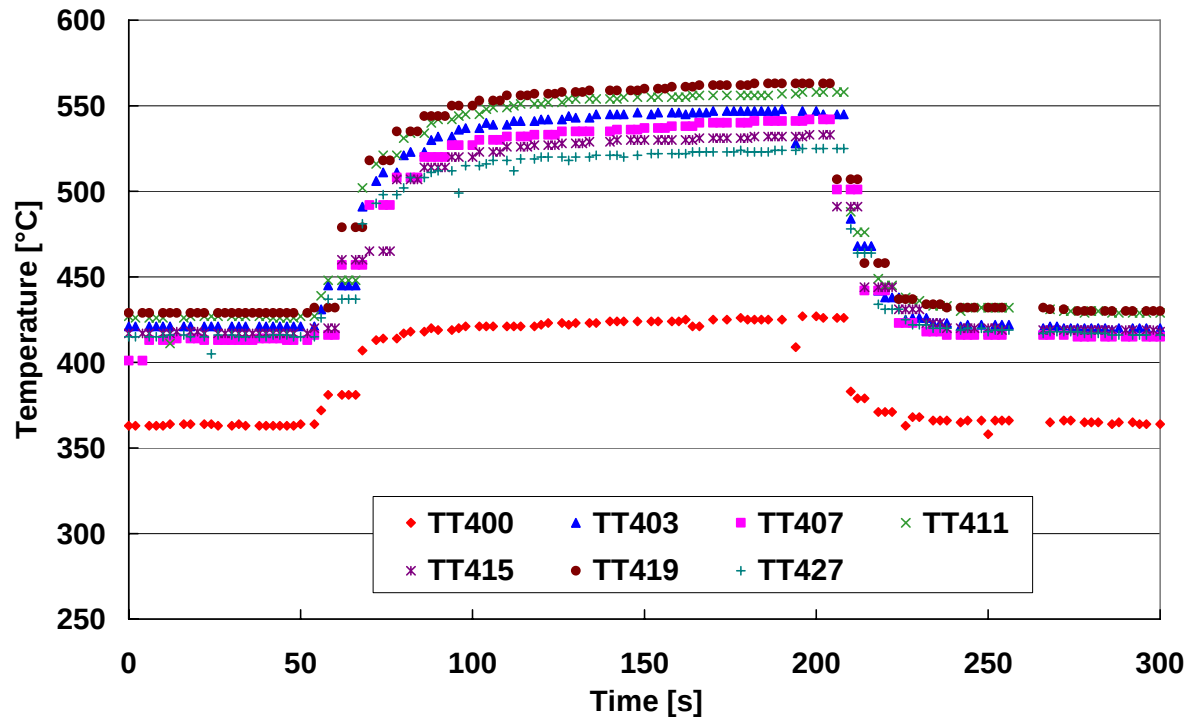


Fig. 26 – Thermocouple Temperatures on 7 TS Positions (30LOFA09-07-98)

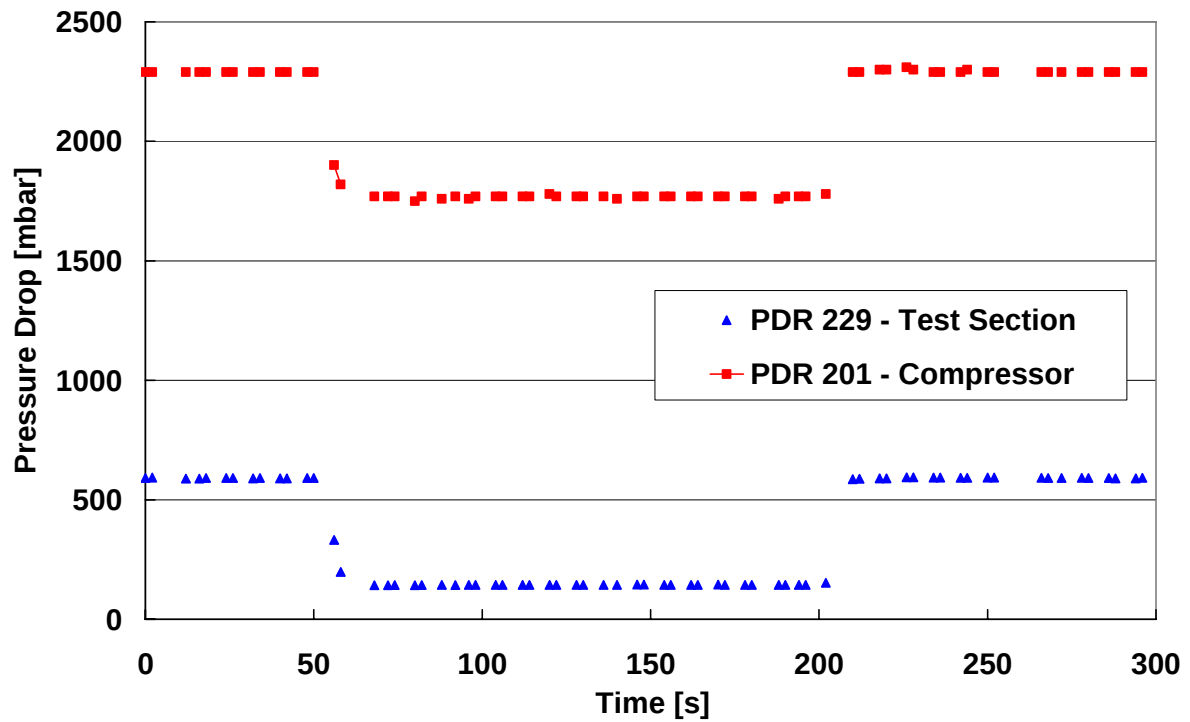


Fig. 27 – TS and Compressor Pressure Drop (30LOFA09-07-98)

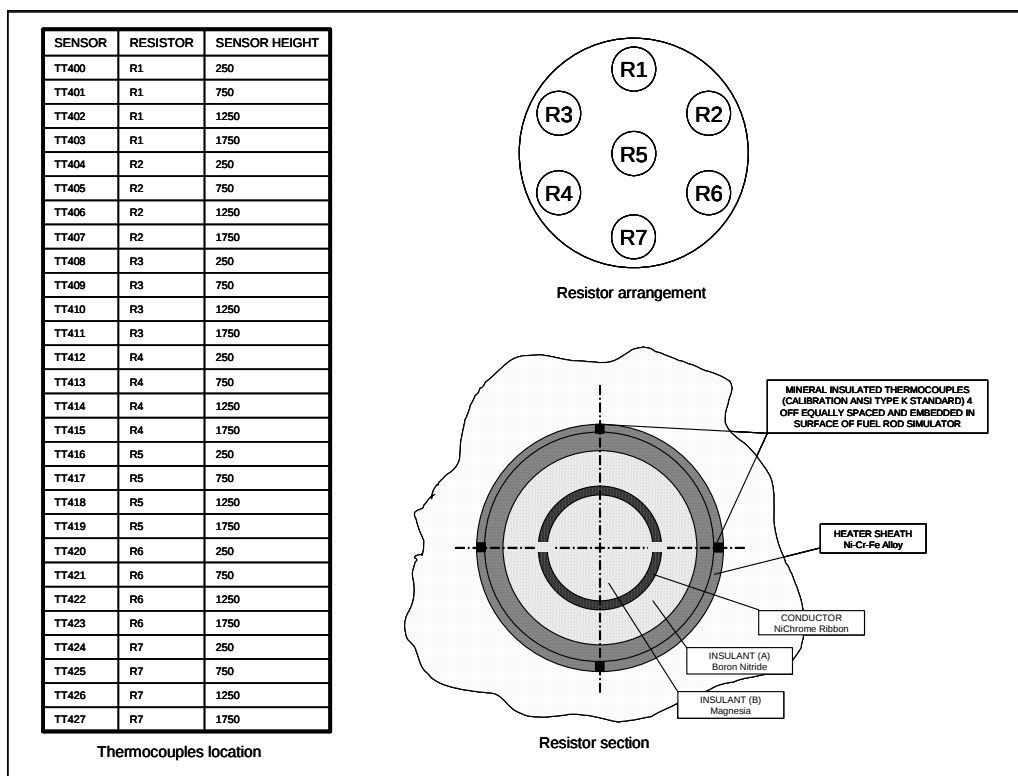


Fig. 28 - Test Section Thermocouples Location

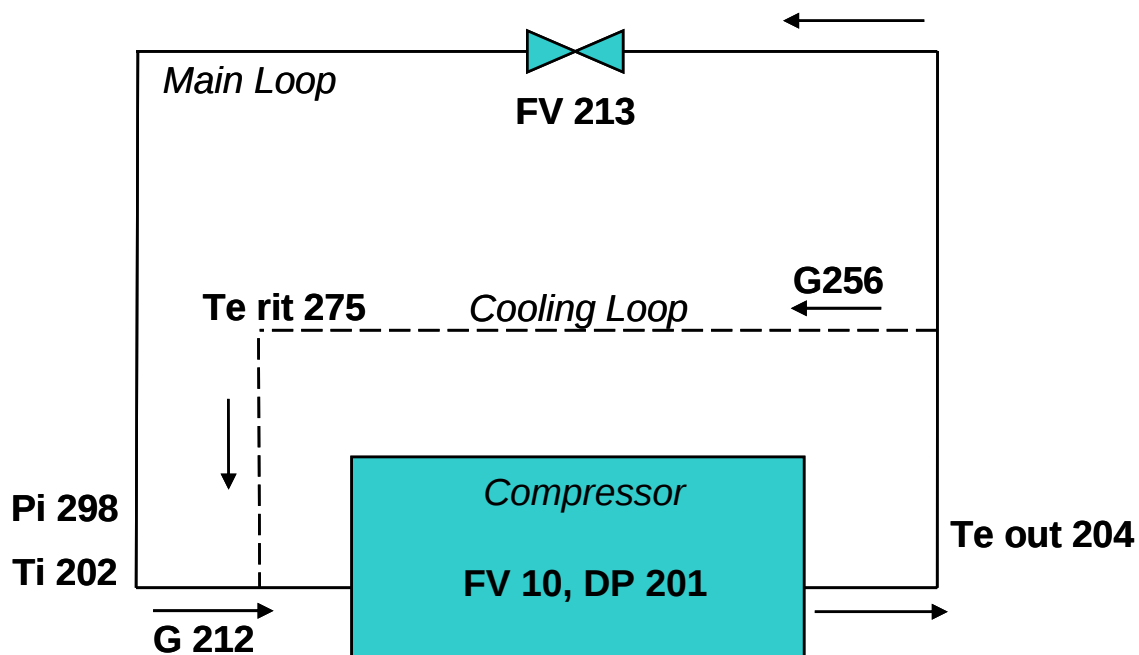
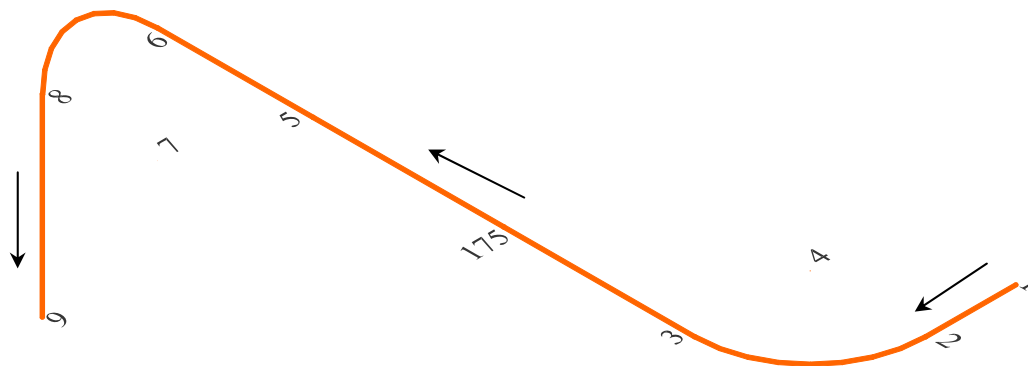


Fig. 29 – Scheme of the Compressor Characterization Test

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Appendix A: Loop Noding for Thermo-mechanical Analysis

LINE A

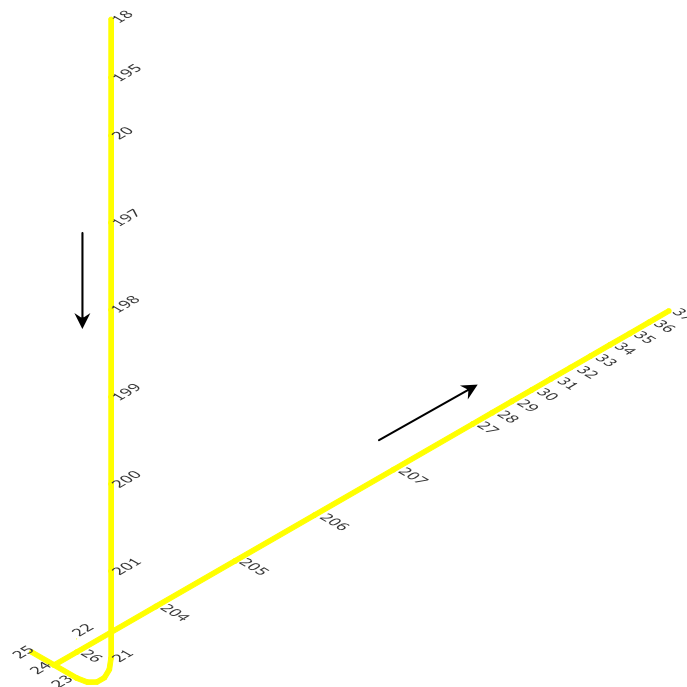


Element	Material	NODE	X	Y	Z	Outside Diameter	Pipe Thickness	Bend Radius	Insulator Thickness	Temp	Press
Type	n°	n°	m	m	m	m	m	m	mm	°C	MPa
D	1	1	2.3338	-4.5909	11.6520	0.1413	9.52E-03		160	520	10
C	1	2	2.3338	-4.7398	11.6520	0.1413	9.52E-03		160	520	10
C	1	3	2.1433	-4.9303	11.6520	0.1413	9.52E-03		160	520	10
RC	1	4	2.1433	-4.7398	11.6520	0.1413	9.52E-03	0.1905	160	520	10
D	1	175	1.8285	-4.9303	11.6520	0.1413	9.52E-03		160	520	10
D	1	5	1.5138	-4.9303	11.6520	0.1413	9.52E-03		160	520	10
C	1	6	1.2576	-4.9303	11.6520	0.1413	9.52E-03		160	520	10
C	1	8	1.0671	-4.9303	11.4620	0.1413	9.52E-03		160	520	10
RC	1	7	1.2576	-4.9303	11.4620	0.1413	9.52E-03	0.1905	160	520	10
D	1	9	1.0671	-4.9303	11.1420	0.1413	9.52E-03		160	520	10

LEGEND:

D	→	Straight Element
C	→	Curve Element
RC	→	Bending Center
T	→	T-Shape Element

LINE B

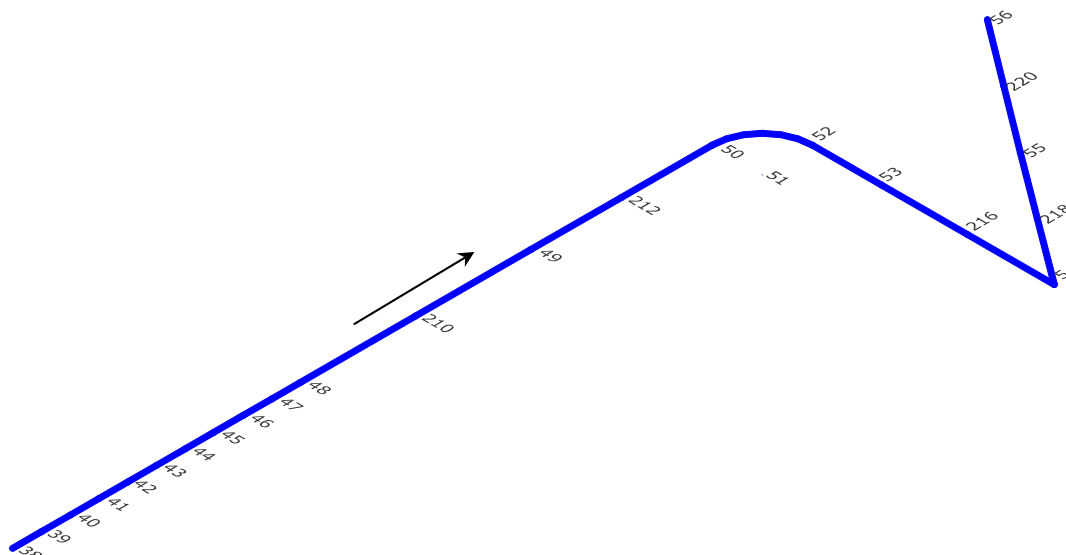


Element	Material	NODE	X	Y	Z	Outside Diam.	Pipe Thick	Bend Radius	Insulator Thick.	Temp	Press
Type	n°	n°	m	m	m	m	m	m	mm	°C	MPa
D	2	18	1.0671	-4.9303	5.9061	0.1413	9.52E-03		100	240	10
D	2	195	1.0671	-4.9303	5.6828	0.1413	9.52E-03		100	240	10
D	2	20	1.0671	-4.9303	5.4595	0.1140	8.56E-03		100	240	10
D	2	197	1.0671	-4.9303	5.1248	0.1140	8.56E-03		100	240	10
D	2	198	1.0671	-4.9303	4.7900	0.1140	8.56E-03		100	240	10
D	2	199	1.0671	-4.9303	4.4553	0.1140	8.56E-03		100	240	10



D	2	200	1.0671	-4.9303	4.1206	0.1140	8.56E-03		100	240	10
D	2	201	1.0671	-4.9303	3.7859	0.1140	8.56E-03		100	240	10
C	2	21	1.0671	-4.9303	3.4512	0.1140	8.56E-03		100	240	10
RC	2	22	0.91488	-4.9303	3.4512	0.1140	8.56E-03	0.1522	100	240	10
T	2	23	0.91488	-4.9303	3.2990	0.1140	8.56E-03		100	240	10
T	2	24	0.81561	-4.9303	3.2990	0.1140	8.56E-03		100	240	10
T	2	26	0.81561	-4.8310	3.2990	0.1140	8.56E-03		100	240	10
T	2	25	0.71635	-4.9303	3.2990	0.1413	8.56E-03		100	240	10
D	2	204	0.81561	-4.4803	3.2990	0.1413	9.52E-03		100	240	10
D	2	205	0.81561	-4.1295	3.2990	0.1413	9.52E-03		100	240	10
D	2	206	0.81561	-3.7787	3.2990	0.1413	9.52E-03		100	240	10
D	2	207	0.81561	-3.4279	3.2990	0.1413	9.52E-03		100	240	10
D	2	27	0.81561	-3.0771	3.2990	0.1413	9.52E-03		100	240	10
D	2	28	0.81561	-2.9903	3.2990	0.1413	9.52E-03		100	240	10
D	2	29	0.81561	-2.9034	3.2990	0.1413	9.52E-03		100	240	10
D	2	30	0.81561	-2.8166	3.2990	0.1413	9.52E-03		100	240	10
D	2	31	0.81561	-2.7297	3.2990	0.1413	9.52E-03		100	240	10
D	2	32	0.81561	-2.6429	3.2990	0.1413	9.52E-03		100	240	10
D	2	33	0.81561	-2.5560	3.2990	0.1413	9.52E-03		100	240	10
D	2	34	0.81561	-2.4692	3.2990	0.1413	9.52E-03		100	240	10
D	2	35	0.81561	-2.3823	3.2990	0.1413	9.52E-03		100	240	10
D	2	36	0.81561	-2.2955	3.2990	0.1413	9.52E-03		100	240	10
D	2	37	0.81561	-2.2086	3.2990	0.1413	9.52E-03		100	240	10

LINE C+P



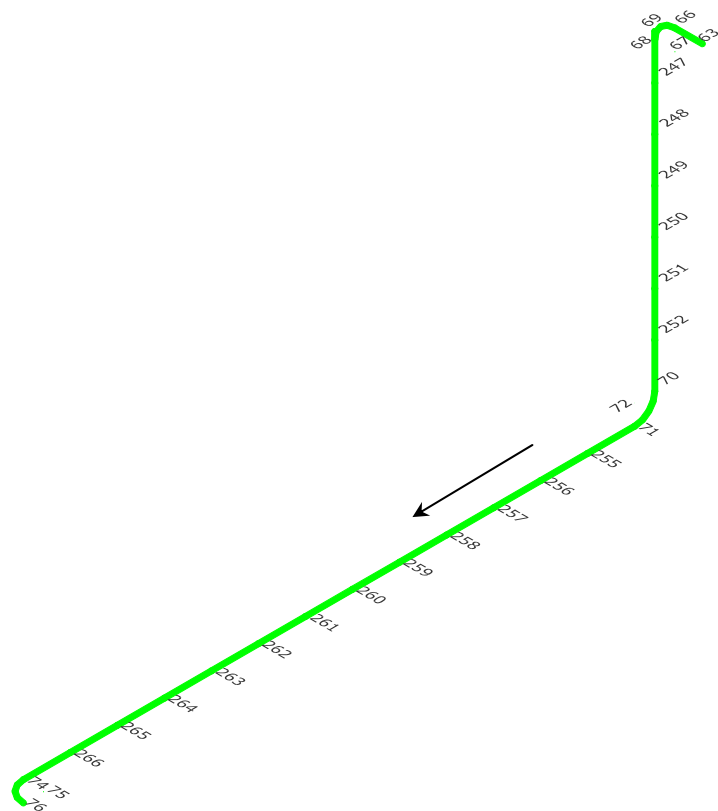
Element	Material	NODE	X	Y	Z	Outside Diam.	Pipe Thick	Bend Radius	Insulator Thick.	Temp	Press
Type	n°	n°	m	m	m	m	m	m	mm	°C	MPa
D	3	38	0.23575	-3.07710	1.2890	0.1140	8.56E-03		60	100	10
D	3	39	0.23575	-2.99030	1.2890	0.1140	8.56E-03		60	100	10
D	3	40	0.23575	-2.90340	1.2890	0.1140	8.56E-03		60	100	10
D	3	41	0.23575	-2.81660	1.2890	0.1140	8.56E-03		60	100	10
D	3	42	0.23575	-2.72970	1.2890	0.1140	8.56E-03		60	100	10
D	3	43	0.23575	-2.64290	1.2890	0.1140	8.56E-03		60	100	10
D	3	44	0.23575	-2.55600	1.2890	0.1140	8.56E-03		60	100	10
D	3	45	0.23575	-2.46920	1.2890	0.1140	8.56E-03		60	100	10
D	3	46	0.23575	-2.38230	1.2890	0.1140	8.56E-03		60	100	10

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D	3	47	0.23575	-2.29550	1.2890	0.1140	8.56E-03		60	100	10
D	3	48	0.23575	-2.20860	1.2890	0.1140	8.56E-03		60	100	10
D	3	210	0.23575	-1.86120	1.2890	0.1140	8.56E-03		60	100	10
D	3	49	0.23575	-1.51380	1.2890	0.1140	8.56E-03		60	100	10
D	3	212	0.23575	-1.24080	1.2890	0.1140	8.56E-03		60	100	10
C	3	50	0.23575	-0.96781	1.2890	0.1140	8.56E-03		60	100	10
C	3	52	0.38795	-0.96781	1.2890	0.1140	8.56E-03		60	100	10
RC	3	51	0.38795	-0.81561	1.2890	0.1140	8.56E-03	0.1522	60	100	10
D	3	53	0.59558	-0.81561	1.2890	6.03E-02	2.77E-03		60	100	10
D	3	216	0.85614	-0.81561	1.2890	6.03E-02	2.77E-03		60	100	10
D	3	54	1.11670	-0.81561	1.2890	6.03E-02	2.77E-03		60	100	10
D	3	218	0.91818	-0.66837	1.2890	6.03E-02	2.77E-03		60	100	10
D	3	55	0.71966	-0.52113	1.2890	6.03E-02	2.77E-03		60	100	10
D	3	220	0.52113	-0.37224	1.2890	0.1140	8.56E-03		60	100	10
D	3	56	0.32260	-0.22334	1.2890	0.1140	8.56E-03		60	100	10

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LINE D

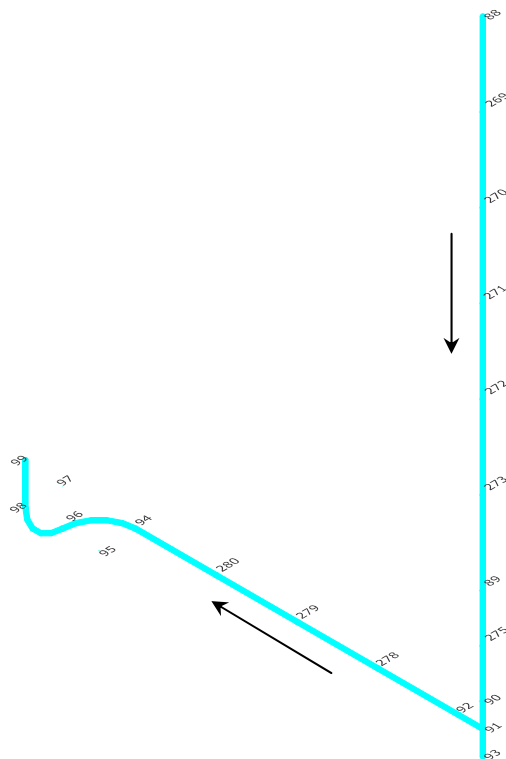


Element	Material	NODE	X	Y	Z	Outside Diam.	Pipe Thick	Bend Radius	Insulator Thick.	Temp	Press
Type	n°	n°	m	m	m	m	m	m	mm	°C	MPa
D	4	63	-0.39705	0.00E+00	5.9061	0.1140	8.56E-03		60	140	10
C	4	66	-0.60468	0.00E+00	5.9061	0.1140	8.56E-03		60	140	10



C	4	68	-0.60468	0.00E+00	5.7539	0.1140	8.56E-03		60	140	10
RC	4	67	-0.75688	0.00E+00	5.7539	0.1140	8.56E-03	0.1522	60	140	10
D	4	69	-0.75688	0.00E+00	5.8069	0.1140	8.56E-03		60	140	10
D	4	247	-0.75688	0.00E+00	5.4704	0.1140	8.56E-03		60	140	10
D	4	248	-0.75688	0.00E+00	5.1338	0.1140	8.56E-03		60	140	10
D	4	249	-0.75688	0.00E+00	4.7973	0.1140	8.56E-03		60	140	10
D	4	250	-0.75688	0.00E+00	4.4608	0.1140	8.56E-03		60	140	10
D	4	251	-0.75688	0.00E+00	4.1243	0.1140	8.56E-03		60	140	10
D	4	252	-0.75688	0.00E+00	3.7878	0.1140	8.56E-03		60	140	10
C	4	70	-0.75688	0.00E+00	3.4512	0.1140	8.56E-03		60	140	10
C	4	72	-0.75688	-0.1522	3.4512	0.1140	8.56E-03		60	140	10
RC	4	71	-0.75688	-0.1522	3.2990	0.1140	8.56E-03	0.1522	60	140	10
D	4	255	-0.75688	-0.50804	3.2990	0.1140	8.56E-03		60	140	10
D	4	256	-0.75688	-0.86388	3.2990	0.1140	8.56E-03		60	140	10
D	4	257	-0.75688	-1.2197	3.2990	0.1140	8.56E-03		60	140	10
D	4	258	-0.75688	-1.5756	3.2990	0.1140	8.56E-03		60	140	10
D	4	259	-0.75688	-1.9314	3.2990	0.1140	8.56E-03		60	140	10
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D	4	261	-0.75688	-2.6431	3.2990	0.1140	8.56E-03		60	140	10
D	4	262	-0.75688	-2.9989	3.2990	0.1140	8.56E-03		60	140	10
D	4	263	-0.75688	-3.3547	3.2990	0.1140	8.56E-03		60	140	10
D	4	264	-0.75688	-3.7106	3.2990	0.1140	8.56E-03		60	140	10
D	4	265	-0.75688	-4.0664	3.2990	0.1140	8.56E-03		60	140	10
D	4	266	-0.75688	-4.4223	3.2990	0.1140	8.56E-03		60	140	10
C	4	74	-0.75688	-4.7781	3.2990	0.1140	8.56E-03		60	140	10
RC	4	75	-0.60468	-4.7781	3.2990	0.1140	8.56E-03	0.1522	60	140	10
C	4	76	-0.60468	-4.9303	3.2990	0.1140	8.56E-03		60	140	10

LINE E

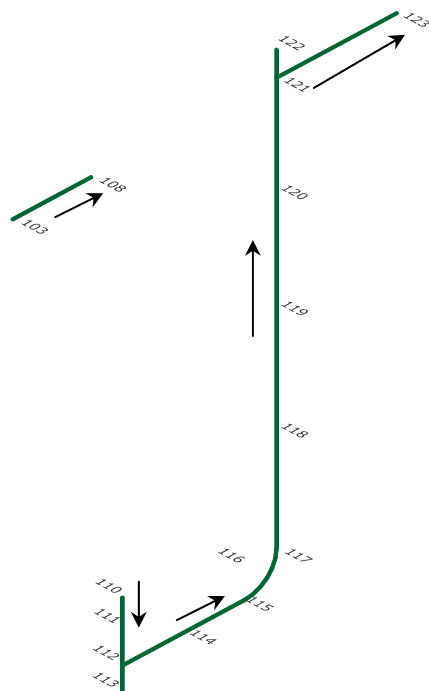


Element	Material	NODE	X	Y	Z	Outside Diam.	Pipe Thick	Bend Radius	Insulator Thick.	Temp	Press
Type	n°	n°	m	m	m	m	m	m	mm	°C	MPa
D	5	88	1.0671	-4.1690	10.7450	0.1140	8.56E-03		160	420	10
D	5	269	1.0671	-4.1690	10.4020	0.1140	8.56E-03		160	420	10
D	5	270	1.0671	-4.1690	10.0590	0.1140	8.56E-03		160	420	10



D	5	271	1.0671	-4.1690	9.7154	0.1140	8.56E-03		160	420	10
D	5	272	1.0671	-4.1690	9.3721	0.1140	8.56E-03		160	420	10
D	5	273	1.0671	-4.1690	9.0288	0.1140	8.56E-03		160	420	10
D	5	89	1.0671	-4.1690	8.6855	0.1140	8.56E-03		160	420	10
D	5	275	1.0671	-4.1690	8.4870	0.1140	8.56E-03		160	420	10
T	5	90	1.0671	-4.1690	8.2885	0.1140	8.56E-03		160	420	10
T	5	91	1.0671	-4.1690	8.1892	0.1140	8.56E-03		160	420	10
T	5	92	0.96781	-4.1690	8.1892	0.1140	8.56E-03		160	420	10
T	5	93	1.0670	-4.1690	8.0899	0.1140	8.56E-03		160	420	10
D	5	278	0.63363	-4.1690	8.1892	0.1140	8.56E-03		160	420	10
D	5	279	0.29944	-4.1690	8.1892	0.1140	8.56E-03		160	420	10
D	5	280	-0.03470	-4.1690	8.1892	0.1140	8.56E-03		160	420	10
C	5	94	-0.36893	-4.1690	8.1892	0.1140	8.56E-03		160	420	10
RC	5	95	-0.36893	-4.3212	8.1892	0.1140	8.56E-03	0.1522	160	420	10
C	5	96	-0.52113	-4.3212	8.1892	0.1140	8.56E-03		160	420	10
RC	5	97	-0.52113	-4.3212	8.3414	0.1140	8.56E-03	0.1522	160	420	10
C	5	98	-0.52113	-4.4734	8.3414	0.1140	8.56E-03		160	420	10
D	5	99	-0.52113	-4.4734	8.5118	0.1140	8.56E-03		160	420	10

LINE F

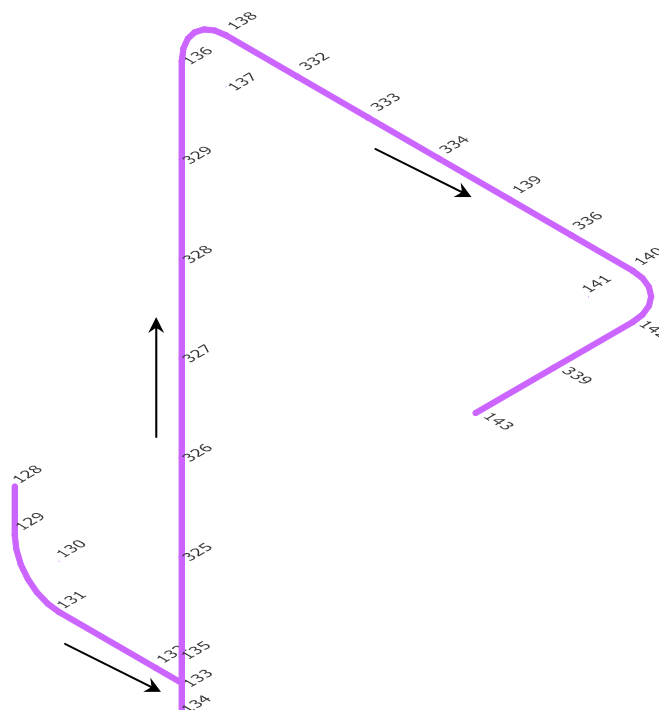


Element	Material	NODE	X	Y	Z	Outside Diam.	Pipe Thick	Bend Radius	Insulator Thick.	Temp	Press
Type	n°	n°	m	m	m	m	m	m	mm	°C	MPa
D	6	103	-0.52113	-4.3179	10.4470	0.1413	9.52E-03		160	530	10
D	6	108	-0.52113	-3.9457	10.4470	0.1413	9.52E-03		160	530	10
D	6	110	-0.52113	-3.7968	8.5118	0.1413	9.52E-03		160	530	10
T	6	111	-0.52113	-3.7968	8.3615	0.1413	9.52E-03		160	530	10

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T	6	112	-0.52113	-3.7968	8.2112	0.1413	9.52E-03		160	530	10
T	6	113	-0.52113	-3.7968	8.0899	0.1413	9.52E-03		160	530	10
T	6	114	-0.52113	-3.6603	8.2112	0.1413	9.52E-03		160	530	10
C	6	115	-0.52113	-3.2169	8.2112	0.1413	9.52E-03		160	530	10
RC	6	116	-0.52113	-3.2169	8.3634	0.1413	9.52E-03		160	530	10
C	6	117	-0.52113	-3.0647	8.3634	0.1413	9.52E-03		160	530	10
D	6	118	-0.52113	-3.0647	8.9153	0.1413	9.52E-03		160	530	10
D	6	119	-0.52113	-3.0647	9.3634	0.1413	9.52E-03		160	530	10
T	6	120	-0.52113	-3.0647	9.9153	0.1413	9.52E-03		160	530	10
T	6	121	-0.52113	-3.0647	10.4470	0.1413	9.52E-03		160	530	10
T	6	122	-0.52113	-3.0647	10.5710	0.1413	9.52E-03		160	530	10
T	6	123	-0.52113	-2.494	10.4470	0.1413	9.52E-03		160	530	10

LINE G



Element	Material	NODE	X	Y	Z	Outside Diam.	Pipe Thick	Bend Radius	Insulator Thick.	Temp	Press
Type	n°	n°	m	m	m	m	m	m	mm	°C	MPa
D	7	128	-0.52113	-2.3327	8.5118	0.1413	9.52E-03		160	420	10
C	7	129	-0.52113	-2.3327	8.3301	0.1413	9.52E-03		160	420	10
RC	7	130	-0.33063	-2.3327	8.3301	0.1413	9.52E-03	0.1905	160	420	10
C	7	131	-0.33063	-2.3327	8.1396	0.1413	9.52E-03		160	420	10
T	7	132	8.69E-02	-2.3327	8.1396	0.1413	9.52E-03		160	420	10



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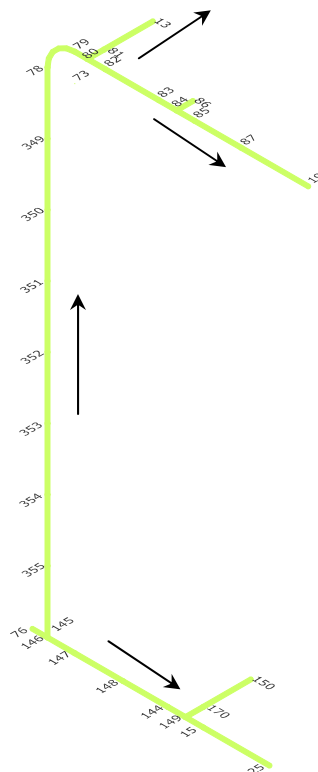
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T	7	133	0.19853	-2.3327	8.1396	0.1413	9.52E-03		160	420	10
T	7	134	0.19853	-2.3327	8.0403	0.1413	9.52E-03		160	420	10
T	7	135	0.19853	-2.3327	8.2388	0.1413	9.52E-03		160	420	10
D	7	325	0.19853	-2.3327	8.6084	0.1413	9.52E-03		160	420	10
D	7	326	0.19853	-2.3327	8.9781	0.1413	9.52E-03		160	420	10
D	7	327	0.19853	-2.3327	9.3477	0.1413	9.52E-03		160	420	10
D	7	328	0.19853	-2.3327	9.7173	0.1413	9.52E-03		160	420	10
D	7	329	0.19853	-2.3327	10.0870	0.1413	9.52E-03		160	420	10
C	7	136	0.19853	-2.3327	10.4570	0.1413	9.52E-03		160	420	10
RC	7	137	0.38903	-2.3327	10.4570	0.1413	9.52E-03	0.1905	160	420	10
C	7	138	0.38903	-2.3327	10.6470	0.1413	9.52E-03		160	420	10
D	7	332	0.69502	-2.3327	10.6470	0.1413	9.52E-03		160	420	10
D	7	333	1.00100	-2.3327	10.6470	0.1413	9.52E-03		160	420	10
D	7	334	1.30700	-2.3327	10.6470	0.1413	9.52E-03		160	420	10
D	7	139	1.61300	-2.3327	10.6470	0.1413	9.52E-03		160	420	10
D	7	336	1.87820	-2.3327	10.6470	0.1413	9.52E-03		160	420	10
C	7	140	2.14330	-2.3327	10.6470	0.1413	9.52E-03		160	420	10
RC	7	141	2.14330	-2.5232	10.6470	0.1413	9.52E-03	0.1905	160	420	10
C	7	142	2.33380	-2.5232	10.6470	0.1413	9.52E-03		160	420	10
D	7	339	2.33380	-2.8622	10.6470	0.1413	9.52E-03		160	420	10
D	7	143	2.33380	-3.2012	10.6470	0.1413	9.52E-03		160	420	10

LINE H



Element	Material	NODE	X	Y	Z	Outside Diam.	Pipe Thick	Bend Radius	Insulator Thick.	Temp	Press
Type	n°	n°	m	m	m	m	m	m	mm	°C	MPa
C	8	78	-0.52113	-4.9303	6.0517	0.1140	8.56E-03		100	240	10
C	8	79	-0.36893	-4.9303	6.2039	0.1140	8.56E-03		100	240	10
RC	8	73	-0.36893	-4.9303	6.0517	0.1140	8.56E-03	0.1522	100	240	10

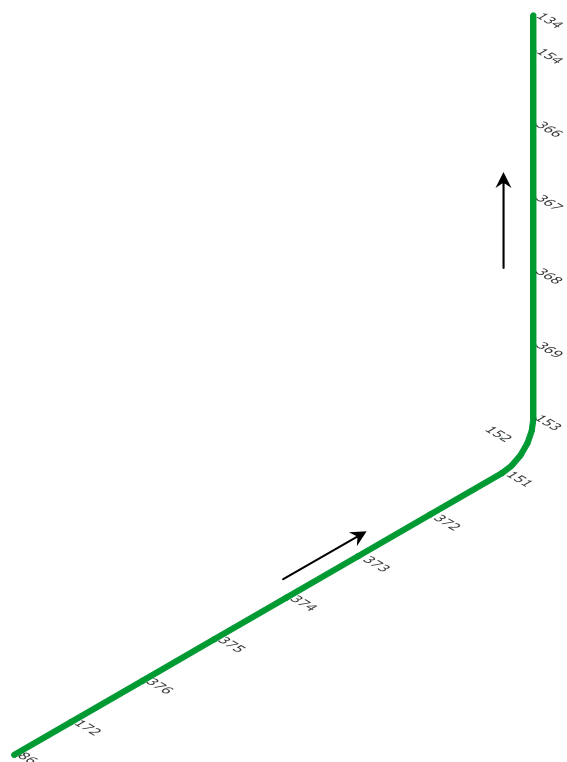
T	8	79	-0.36893	-4.9303	6.2039	0.1140	8.56E-03		100	240	10
T	8	80	-0.29779	-4.9303	6.2039	0.1140	8.56E-03		100	240	10
T	8	81	-0.29779	-4.8391	6.2039	0.1140	8.56E-03		100	240	10
T	8	82	-0.19853	-4.9303	6.2039	0.1140	8.56E-03		100	240	10
T	8	83	9.93E-02	-4.9303	6.2039	0.1140	8.56E-03		100	240	10
T	8	84	0.19853	-4.9303	6.2039	0.1140	8.56E-03		100	240	10
T	8	85	0.29779	-4.9303	6.2039	0.1140	8.56E-03		100	240	10
T	8	86	0.19853	-4.8391	6.2039	0.1140	8.56E-03		100	240	10
D	8	13	-0.29779	-4.5661	6.2039	0.1140	8.56E-03		100	240	10
D	8	81	-0.29779	-4.8391	6.2039	0.1140	8.56E-03		100	240	10
D	8	82	-0.19853	-4.9303	6.2039	0.1140	8.56E-03		100	240	10
D	8	83	9.93E-02	-4.9303	6.2039	0.1140	8.56E-03		100	240	10
D	8	85	0.29779	-4.9303	6.2039	0.1140	8.56E-03		100	240	10
D	8	87	0.55835	-4.9303	6.2039	0.1140	8.56E-03		100	240	10
D	8	19	0.93208	-4.9303	6.2039	0.1140	8.56E-03		100	240	10
D	8	78	-0.52113	-4.9303	6.0517	0.1140	8.56E-03		100	240	10
D	8	349	-0.52113	-4.9303	5.7080	0.1140	8.56E-03		100	240	10
D	8	350	-0.52113	-4.9303	5.3642	0.1140	8.56E-03		100	240	10
D	8	351	-0.52113	-4.9303	5.0204	0.1140	8.56E-03		100	240	10
D	8	352	-0.52113	-4.9303	4.6766	0.1140	8.56E-03		100	240	10
D	8	353	-0.52113	-4.9303	4.3328	0.1140	8.56E-03		100	240	10
D	8	354	-0.52113	-4.9303	3.9891	0.1140	8.56E-03		100	240	10
D	8	355	-0.52113	-4.9303	3.6453	0.1140	8.56E-03		100	240	10
T	8	145	-0.52113	-4.9303	3.3015	0.1140	8.56E-03		100	240	10
T	8	76	-0.60468	-4.9303	3.2990	0.1140	8.56E-03		100	240	10
T	8	146	-0.52113	-4.9303	3.2990	0.1140	8.56E-03		100	240	10
T	8	147	-0.36893	-4.9303	3.2990	0.1140	8.56E-03		100	240	10
D	8	148	-9.93E-02	-4.9303	3.2990	0.1140	8.56E-03		100	240	10
T	8	144	0.14889	-4.9303	3.2990	0.1140	8.56E-03		100	240	10
T	8	149	0.24816	-4.9303	3.2990	0.1140	8.56E-03		100	240	10
T	8	15	0.34742	-4.9303	3.2990	0.1140	8.56E-03		100	240	10
T	8	170	0.24816	-4.8310	3.2990	0.1140	8.56E-03		100	240	10

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D	8	150	0.24816	-4.5661	3.2990	0.1140	8.56E-03		100	240	10
D	8	15	0.34742	-4.9303	3.2990	0.1140	8.56E-03		100	240	10
D	8	26	0.71635	-4.9303	3.2990	0.1140	8.56E-03		100	240	10

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LINE I



Element	Material	NODE	X	Y	Z	Outside Diam.	Pipe Thick	Bend Radius	Insulator Thick.	Temp	Press
Type	n°	n°	m	m	m	m	m	m	mm	°C	MPa
D	9	134	0.19853	-2.3327	8.0403	0.1140	8.56E-03		100	140	10
D	9	154	0.19853	-2.3327	7.8914	0.1140	8.56E-03		100	140	10
D	9	366	0.19853	-2.3327	7.5843	0.1140	8.56E-03		100	140	10
D	9	367	0.19853	-2.3327	7.2773	0.1140	8.56E-03		100	140	10



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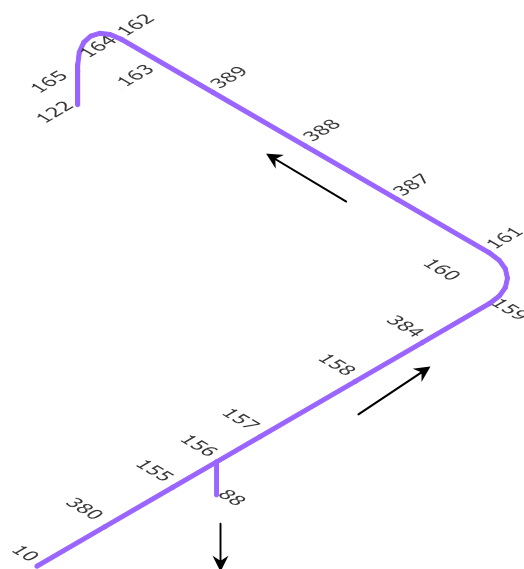
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D	9	368	0.19853	-2.3327	6.9702	0.1140	8.56E-03		100	140	10
D	9	369	0.19853	-2.3327	6.6632	0.1140	8.56E-03		100	140	10
C	9	151	0.19853	-2.4849	6.2039	0.1140	8.56E-03		100	140	10
RC	9	152	0.19853	-2.4849	6.3561	0.1140	8.56E-03	0.1522	100	140	10
C	9	153	0.19853	-2.3327	6.3561	0.1140	8.56E-03		100	140	10
D	9	372	0.19853	-2.8317	6.2039	0.1140	8.56E-03		100	140	10
D	9	373	0.19853	-3.1786	6.2039	0.1140	8.56E-03		100	140	10
D	9	374	0.19853	-3.5255	6.2039	0.1140	8.56E-03		100	140	10
D	9	375	0.19853	-3.8724	6.2039	0.1140	8.56E-03		100	140	10
D	9	376	0.19853	-4.2192	6.2039	0.1140	8.56E-03		100	140	10
D	9	172	0.19853	-4.5661	6.2039	0.1140	8.56E-03		100	140	10
D	9	86	0.19853	-4.8391	6.2039	0.1140	8.56E-03		100	140	10

LINE L



Element	Material	NODE	X	Y	Z	Outside Diam.	Pipe Thick	Bend Radius	Insulator Thick.	Temp	Press
Type	n°	n°	m	m	m	m	m	m	mm	°C	MPa
D	10	10	1.0671	-4.7953	10.8440	0.1140	8.56E-03		160	420	10
D	10	380	1.0671	-4.5583	10.8440	0.1140	8.56E-03		160	420	10
T	10	155	1.0671	-4.3212	10.8440	0.1140	8.56E-03		160	420	10
T	10	156	1.0671	-4.1690	10.8440	0.1140	8.56E-03		160	420	10
T	10	157	1.0671	-4.0168	10.8440	0.1140	8.56E-03		160	420	10
T	10	88	1.0671	-4.1690	10.7450	0.1140	8.56E-03		160	420	10
D	10	158	1.0671	-3.6851	10.8440	0.1140	8.56E-03		160	420	10
D	10	384	1.0671	-3.4510	10.8440	0.1140	8.56E-03		160	420	10



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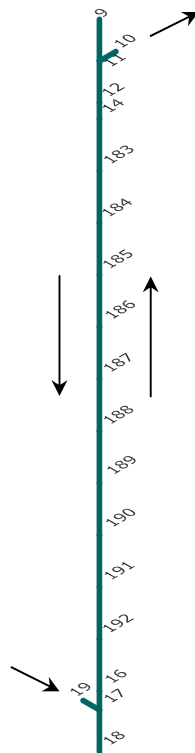
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C	10	159	1.0671	-3.2169	10.8440	0.1140	8.56E-03		160	420	10
RC	10	160	0.91488	-3.2169	10.8440	0.1140	8.56E-03	0.1522	160	420	10
C	10	161	0.91488	-3.0647	10.8440	0.1140	8.56E-03		160	420	10
D	10	387	0.59392	-3.0647	10.8440	0.1140	8.56E-03		160	420	10
D	10	388	0.27297	-3.0647	10.8440	0.1140	8.56E-03		160	420	10
D	10	389	-4.80E-02	-3.0647	10.8440	0.1140	8.56E-03		160	420	10
C	10	162	-0.36893	-3.0647	10.8440	0.1140	8.56E-03		160	420	10
RC	10	163	-0.36893	-3.0647	10.6920	0.1140	8.56E-03		160	420	10
C	10	164	-0.52113	-3.0647	10.6920	0.1140	8.56E-03		160	420	10
D	10	165	-0.52113	-3.0647	10.6710	0.1140	8.56E-03		160	420	10
D	10	122	-0.52113	-3.0647	10.5710	0.1140	8.56E-03		160	420	10

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ECONOMIZER

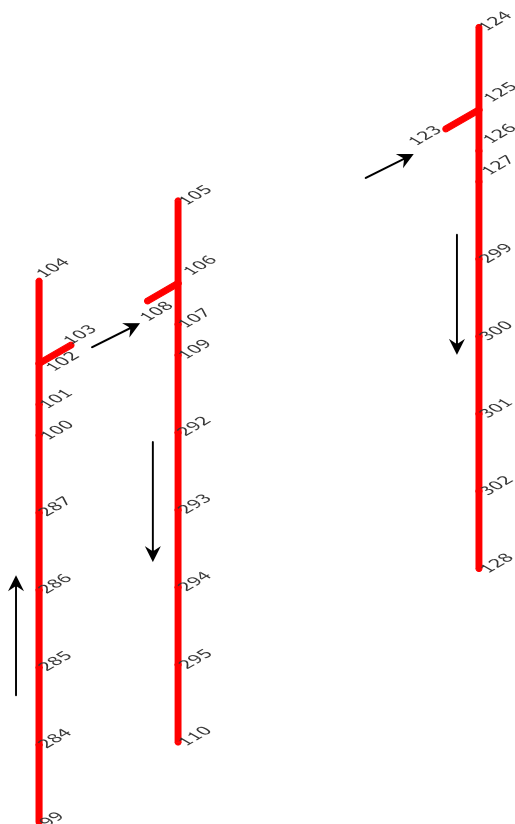


Element	Material	NODE	X	Y	Z	Outside Diam.	Pipe Thick	Bend Radius	Insulator Thick.	Temp	Press
Type	n°	n°	m	m	m	m	m	m	mm	°C	MPa
T	13	9	1.0671	-4.9303	11.1420	0.31	2.00E-02		160	520	10
T	13	10	1.0671	-4.7953	10.8440	0.31	2.00E-02		160	420	10
T	13	11	1.0671	-4.9303	10.8440	0.31	2.00E-02		160	498	10
T	13	12	1.0671	-4.9303	10.5470	0.31	2.00E-02		160	476	10



D	13	13	-0.29779	-4.5661	6.2039	0.31	2.00E-02		160	140	10
D	13	14	1.0671	-4.9303	10.4310	0.31	2.00E-02		160	454	10
D	13	183	1.0671	-4.9303	10.0590	0.31	2.00E-02		160	410	10
D	13	184	1.0671	-4.9303	9.6871	0.31	2.00E-02		160	366	10
D	13	185	1.0671	-4.9303	9.3151	0.31	2.00E-02		160	322	10
D	13	186	1.0671	-4.9303	8.9431	0.31	2.00E-02		160	278	10
D	13	187	1.0671	-4.9303	8.5710	0.31	2.00E-02		160	234	10
D	13	188	1.0671	-4.9303	8.1990	0.31	2.00E-02		160	190	10
D	13	189	1.0671	-4.9303	7.8270	0.31	2.00E-02		160	146	10
D	13	190	1.0671	-4.9303	7.4550	0.31	2.00E-02		160	102	10
D	13	191	1.0671	-4.9303	7.0830	0.31	2.00E-02		160	58	10
D	13	192	1.0671	-4.9303	6.7110	0.31	2.00E-02		160	14	10
T	13	16	1.0671	-4.9303	6.3389	0.31	2.00E-02		160	212	10
T	13	17	1.0671	-4.9303	6.2039	0.31	2.00E-02		160	190	10
T	13	18	1.0671	-4.9303	5.9061	0.31	2.00E-02		160	240	10
T	13	19	0.93208	-4.9303	6.2039	0.31	2.00E-02		160	140	10

RE-HEATER

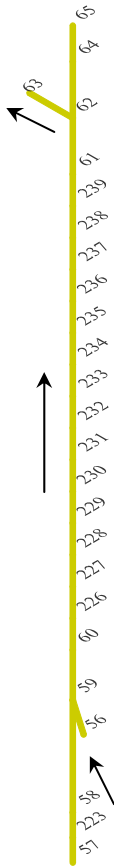


Element	Material	NODE	X	Y	Z	Outside Diam.	Pipe Thick	Bend Radius	Insulator Thick.	Temp	Press
Type	n°	n°	m	m	m	m	m	m	mm	°C	MPa
D	14	99	-0.52113	-4.4734	8.5118	0.31	2.00E-02		160	420	10
D	14	284	-0.52113	-4.4734	8.8382	0.31	2.00E-02		160	420	10



D	14	285	-0.52113	-4.4734	9.1646	0.31	2.00E-02		160	420	10
D	14	286	-0.52113	-4.4734	9.4910	0.31	2.00E-02		160	420	10
D	14	287	-0.52113	-4.4734	9.8174	0.31	2.00E-02		160	420	10
D	14	100	-0.52113	-4.4734	10.1440	0.31	2.00E-02		160	420	10
T	14	101	-0.52113	-4.4734	10.2740	0.31	2.00E-02		160	420	10
T	14	102	-0.52113	-4.4734	10.4470	0.31	2.00E-02		160	457	10
T	14	103	-0.52113	-4.3179	10.4470	0.31	2.00E-02		160	457	10
T	14	104	-0.52113	-4.4734	10.7950	0.31	2.00E-02		160	457	10
T	14	105	-0.52113	-3.7968	10.7950	0.31	2.00E-02		160	457	10
T	14	106	-0.52113	-3.7968	10.4470	0.31	2.00E-02		160	457	10
T	14	107	-0.52113	-3.7968	10.2740	0.31	2.00E-02		160	457	10
T	14	108	-0.52113	-3.9457	10.4470	0.31	2.00E-02		160	457	10
D	14	109	-0.52113	-3.7968	10.1440	0.31	2.00E-02		160	457	10
D	14	292	-0.52113	-3.7968	9.8174	0.31	2.00E-02		160	457	10
D	14	293	-0.52113	-3.7968	9.4910	0.31	2.00E-02		160	457	10
D	14	294	-0.52113	-3.7968	9.1646	0.31	2.00E-02		160	457	10
D	14	295	-0.52113	-3.7968	8.8382	0.31	2.00E-02		160	457	10
D	14	110	-0.52113	-3.7968	8.5118	0.31	2.00E-02		160	494	10
T	14	123	-0.52113	-2.4940	10.4470	0.31	2.00E-02		160	494	10
T	14	124	-0.52113	-2.3327	10.7950	0.31	2.00E-02		160	494	10
T	14	125	-0.52113	-2.3327	10.4470	0.31	2.00E-02		160	494	10
T	14	126	-0.52113	-2.3327	10.2740	0.31	2.00E-02		160	494	10
D	14	127	-0.52113	-2.3327	10.1440	0.31	2.00E-02		160	494	10
D	14	299	-0.52113	-2.3327	9.8174	0.31	2.00E-02		160	494	10
D	14	300	-0.52113	-2.3327	9.4910	0.31	2.00E-02		160	494	10
D	14	301	-0.52113	-2.3327	9.1646	0.31	2.00E-02		160	494	10
D	14	302	-0.52113	-2.3327	8.8382	0.31	2.00E-02		160	494	10
D	14	128	-0.52113	-2.3327	8.5118	0.31	2.00E-02		160	530	10

TANK



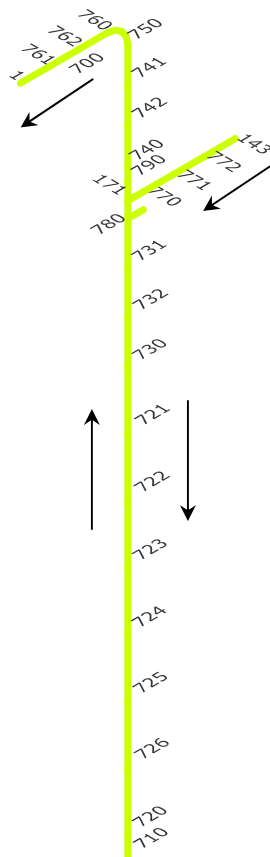
Element	Material	NODE	X	Y	Z	Outside Diam.	Pipe Thick	Bend Radius	Insulator Thick.	Temp	Press
Type	n°	n°	m	m	m	m	m	m	mm	°C	MPa
D	15	57	0.00E+00	0.00E+00	0.00E+00	0.89	4.50E-02		160	100	10



D	15	223	0.00E+00	0.00E+00	0.19853	0.89	4.50E-02		160	100	10
T	15	56	0.3226	-0.22334	1.2890	0.89	4.50E-02		160	100	10
T	15	58	0.00E+00	0.00E+00	0.39705	0.89	4.50E-02		160	100	10
T	15	59	0.00E+00	0.00E+00	1.2890	0.89	4.50E-02		160	100	10
T	15	60	0.00E+00	0.00E+00	1.6860	0.89	4.50E-02		160	100	10
D	15	226	0.00E+00	0.00E+00	1.9376	0.89	4.50E-02		160	100	10
D	15	227	0.00E+00	0.00E+00	2.1891	0.89	4.50E-02		160	100	10
D	15	228	0.00E+00	0.00E+00	2.4407	0.89	4.50E-02		160	100	10
D	15	229	0.00E+00	0.00E+00	2.6923	0.89	4.50E-02		160	100	10
D	15	230	0.00E+00	0.00E+00	2.9438	0.89	4.50E-02		160	100	10
D	15	231	0.00E+00	0.00E+00	3.1954	0.89	4.50E-02		160	100	10
D	15	232	0.00E+00	0.00E+00	3.4470	0.89	4.50E-02		160	100	10
D	15	233	0.00E+00	0.00E+00	3.6985	0.89	4.50E-02		160	100	10
D	15	234	0.00E+00	0.00E+00	3.9501	0.89	4.50E-02		160	100	10
D	15	235	0.00E+00	0.00E+00	4.2016	0.89	4.50E-02		160	100	10
D	15	236	0.00E+00	0.00E+00	4.4532	0.89	4.50E-02		160	100	10
D	15	237	0.00E+00	0.00E+00	4.7048	0.89	4.50E-02		160	100	10
D	15	238	0.00E+00	0.00E+00	4.9563	0.89	4.50E-02		160	100	10
D	15	239	0.00E+00	0.00E+00	5.2079	0.89	4.50E-02		160	100	10
T	15	61	0.00E+00	0.00E+00	5.4595	0.89	4.50E-02		160	100	10
T	15	62	0.00E+00	0.00E+00	5.9061	0.89	4.50E-02		160	140	10
T	15	63	-0.39705	0.00E+00	5.9061	0.89	4.50E-02		160	140	10
T	15	64	0.00E+00	0.00E+00	6.3528	0.89	4.50E-02		160	140	10
D	15	65	0.00E+00	0.00E+00	6.6382	0.89	4.50E-02		160	140	10

ENEA	Centro Ricerche Bologna	Sigla di identificazione FPN – P9L7-001	Rev. 0	Distrib. R	Pag. 80	di 91
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TEST SECTION



Element	Material	NODE	X	Y	Z	Outside Diam.	Pipe Thick	Bend Radius	Insulator Thick.	Temp	Press
Type	n°	n°	m	m	m	m	m	m	mm	°C	MPa
D	17	1	2.3338	-4.5909	11.6520	8.89E-02	7.62E-03		160	520	10



D	17	761	2.3338	-4.4037	11.6520	8.89E-02	7.62E-03		160	520	10
D	17	762	2.3338	-4.2166	11.6520	8.89E-02	7.62E-03		160	520	10
C	17	760	2.3338	-4.0294	11.6520	8.89E-02	7.62E-03		160	520	10
C	17	750	2.3338	-3.8961	11.5190	8.89E-02	7.62E-03		160	520	10
RC	17	700	2.3338	-4.0294	11.5190	8.89E-02	7.62E-03	0.1333	160	520	10
D	17	741	2.3338	-3.8961	11.2920	8.89E-02	7.62E-03		160	520	10
D	17	742	2.3338	-3.8961	11.0660	8.89E-02	7.62E-03		160	520	10
D	17	740	2.3338	-3.8961	10.8400	0.1413	1.91E-02		160	520	10
T	17	790	2.3338	-3.8961	10.7470	0.1413	1.91E-02		160	520	10
T	17	171	2.3338	-3.8961	10.6470	0.1413	1.91E-02		160	520	10
T	17	770	2.3338	-3.7961	10.6470	0.1413	1.91E-02		160	520	10
T	17	780	2.3338	-3.7961	10.5470	0.1413	1.91E-02		160	520	10
D	17	771	2.3338	-3.5978	10.6470	8.89E-02	7.62E-03		160	520	10
D	17	772	2.3338	-3.3995	10.6470	8.89E-02	7.62E-03		160	520	10
D	17	143	2.3338	-3.2012	10.6470	8.89E-02	7.62E-03		160	520	10
D	17	780	2.3338	-3.8961	10.5470	0.1413	1.91E-02		160	520	10
D	17	731	2.3338	-3.8961	10.2690	0.1413	1.91E-02		160	520	10
D	17	732	2.3338	-3.8961	9.9917	0.1413	1.91E-02		160	520	10
D	17	730	2.3338	-3.8961	9.7140	0.1413	1.91E-02		160	520	10
D	17	721	2.3338	-3.8961	9.3407	8.89E-02	7.62E-03		160	520	10
D	17	722	2.3338	-3.8961	8.9674	8.89E-02	7.62E-03		160	520	10
D	17	723	2.3338	-3.8961	8.5941	8.89E-02	7.62E-03		160	520	10
D	17	724	2.3338	-3.8961	8.2209	8.89E-02	7.62E-03		160	520	10
D	17	725	2.3338	-3.8961	7.8476	8.89E-02	7.62E-03		160	520	10
D	17	726	2.3338	-3.8961	7.4743	8.89E-02	7.62E-03		160	520	10
D	17	720	2.3338	-3.8961	7.1010	8.89E-02	7.62E-03		160	520	10
D	17	710	2.3338	-3.8961	6.9770	8.89E-02	7.62E-03		160	520	10

 Centro Ricerche Bologna	Sigla di identificazione FPN – P9L7-001	Rev. 0	Distrib. R	Pag. 82	di 91
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Appendix B: HE-FUS3 Experimental Data



HE-FUS3 Steady State Tests	TR 218	TR 215	TR 217	TR 216	FIC 228X	TR 239	TIC 242X	TR 267	TR 266	TIC 242W	TR 202	TR 204	PDR 201	FIC 212W	FIC 212X	FIC 228W	FIC 228Y	ZR 235	ZR 213	ZR 234	TR 220
1ST24-06-98	134.00	88.00	306.00	251.00	795.04	140.00	75.00	14.00	102.00	75.00	78.00	99.00	233.00	449.83	802.61	699.71	1.10	-3.00	101.00	-4.00	242.00
2ST24-06-98	140.00	94.00	307.00	254.00	802.21	146.00	75.03	14.00	102.00	75.00	78.60	99.90	235.20	449.83	809.63	699.71	1.10	-3.00	101.00	-4.00	244.80
4ST24-06-98	138.00	96.00	307.00	256.00	623.17	145.00	75.04	15.00	108.00	75.00	78.00	104.00	270.00	449.83	627.93	699.71	0.50	-3.00	70.00	-4.00	246.00
5ST24-06-98	152.40	96.00	366.40	296.20	791.90	159.40	74.99	15.00	104.00	75.00	78.00	99.00	234.00	449.83	799.32	699.71	1.10	-3.00	101.00	-4.00	284.00
6ST24-06-98	165.00	95.00	424.00	340.00	787.84	173.00	75.01	15.00	106.00	75.00	78.00	99.00	237.20	449.83	795.81	699.71	1.10	-3.00	101.00	-4.00	327.85
7ST-06-98	185.00	94.00	415.00	360.00	806.04	193.00	75.00	11.00	109.00	75.00	78.00	99.00	232.00	449.83	818.36	699.71	1.10	-3.00	102.00	38.00	349.00
8ST-06-98	185.00	94.00	415.00	360.00	807.01	193.00	74.98	12.00	109.00	75.00	78.00	99.00	232.50	449.83	818.26	699.71	1.10	-3.00	101.50	37.30	349.00
9ST-06-98	186.00	95.00	416.00	361.50	807.07	194.00	75.00	16.00	107.00	75.00	77.50	99.00	231.00	449.83	817.51	699.71	1.10	-3.00	101.00	38.00	350.00
40%ST19-02-99	230.00	90.00	521.00	460.00	352.07	234.00	75.00	5.00	137.00	75.00	74.00	99.00	112.40	359.86	359.36	699.71	1.10	-4.00	88.00	47.70	455.00
30%ST19-02-99	204.00	89.00	467.00	408.00	352.00	208.00	75.00	8.00	131.00	75.00	74.00	98.00	112.40	360.00	360.00	700.00	1.10	-4.00	88.00	42.00	404.00

Tab. B1 – Steady State Tests (cont'd)



HE-FUS3 Steady State Tests	TR 221	TR 226	TIC 222X	TIC 222W	TIC 222Y	TR 225	TIC 223X	TIC 223W	TIC 223Y	TR 224	TIC 232X	TIC 232W	TR 233	TR 241	TR 236	TR 297	TIC 242Y	TIC 232Y	ST 270	PR 298	PR 206	PR 227	PDR 229	FIC 212Y
1ST24-06-98	250.00	243.95	269.88	269.97	0.38	269.00	300.04	300.00	0.57	291.00	301.07	499.99	392.00	76.00	303.00	268.00	0.17	-0.05	127.00	47.00	50.00	50.00	568.00	0.72
2ST24-06-98	253.00	246.30	270.00	269.97	0.30	270.00	299.96	300.00	0.56	291.00	301.23	499.99	398.00	76.00	303.10	268.80	0.20	-0.05	128.60	48.00	51.00	50.00	573.10	0.72
4ST24-06-98	255.00	248.00	269.93	269.97	0.23	270.00	299.89	300.00	0.44	291.00	301.14	499.99	402.00	76.00	303.00	269.00	0.13	-0.05	143.00	48.00	51.00	50.00	360.00	0.72
5ST24-06-98	286.60	284.80	274.15	269.97	-0.05	282.20	300.16	300.00	0.37	291.80	301.55	499.99	466.80	75.60	303.60	272.80	0.24	-0.05	143.00	48.00	51.00	51.00	597.60	0.72
6ST24-06-98	331.85	328.85	320.07	269.97	-0.05	328.71	310.28	300.00	-0.05	311.86	310.75	300.00	531.29	75.14	313.57	318.86	0.28	-0.05	143.00	48.00	51.00	51.00	632.29	0.72
7ST-06-98	358.00	351.00	348.41	269.97	-0.05	357.00	342.74	300.00	-0.05	344.00	300.00	300.00	503.00	75.00	346.00	346.00	0.31	0.04	111.00	48.00	51.00	51.00	655.00	0.72
8ST-06-98	358.00	351.00	348.36	269.97	-0.05	357.00	342.71	300.00	-0.05	344.00	299.89	300.00	507.80	75.00	346.00	346.80	0.31	0.63	115.80	48.00	51.00	51.00	655.70	0.72
9ST-06-98	359.00	351.00	348.85	269.97	-0.05	358.00	343.91	300.00	-0.05	345.00	299.96	300.00	526.00	75.00	348.00	348.00	0.35	0.64	143.00	48.00	51.00	51.00	659.00	0.72
40%ST19-02-99	448.00	455.00	445.65	419.97	-0.05	456.00	432.86	419.97	-0.05	433.00	350.06	349.99	392.00	72.00	433.60	442.60	0.39	0.51	181.40	22.00	23.00	24.00	466.60	0.55
30%ST19-02-99	399.00	403.00	420.00	420.00	0.10	423.00	420.00	420.00	0.05	417.00	350.00	350.00	280.00	72.00	421.00	417.00	0.51	0.68	141.82	22.00	24.00	24.00	441.00	0.79

Tab. B1 – Steady State Tests

[illegible]

Tab. B3 – Transient Test 30LOFA09-07-98 (cont'd)

[illegible]

Tab. B3 – Transient Test 30LOFA09-07-98 (cont'd)

[illegible]

Tab. B3 – Transient Test 30LOFA09-07-98

Compressor Characterization Tests 14/03/98									
FV10	FV 213	G 212	DP 201	Ti 202	Pi 298	Te out 204	Tcusc 276	Te rit 275	G 256
rpm	%	kg/s	bar	°C	bar ass	°C	°C	°C	kg/s
10000 rpm (55.5%)									
	100	0,162	1,46	79,7	49,6	85,3	46,4		0,052
	80	0,157	1,49	79,3	49,7	85,4	46,9		0,053
	70	0,147	1,55	79,3	49,6	85,9	47,1		0,054
	60	0,132	1,66	79,3	49,4	86,6	47,4		0,056
	50	0,112	1,81	78,1	49,2	87,2	47,8		0,058
	40	0,087	1,98	74,9	48,9	87,9	48,2		0,061
12000 (66.6%)									
	100	0,193	2,07	80,3	49,6	93,6	52		0,063
	80	0,188	2,12	79,7	49,6	94,7	53,3		0,064
	70	0,176	2,2	79,3	49,6	95,5	53,8		0,065
	60	0,158	2,36	79	49,3	97,3	54,6		0,067
	50	0,131	2,56	79,1	49	100,5	55,5		0,070
	40	0,102	2,76	77,1	48,8	104	56,6		0,073
13000 (72.2%)									
	100	0,211	2,42	79,7	49,7	99,3	56,9		0,068
	80	0,204	2,47	79,6	49,6	100,1	57,6		0,069
	70	0,192	2,58	79,3	49,6	101,5	58,4		0,070
	60	0,171	2,74	79,1	49,4	104,3	59,3		0,072
	50	0,143	3	79,1	49,1	108,1	60,3		0,076
14000 (77.7 %)									
	100	0,228	2,8	79,9	49,8	105,3	61,6		0,073
	80	0,22	2,86	79,6	49,8	106,2	62,1		0,074
	70	0,206	3	79,4	49,7	108	62,8		0,076
	60	0,187	3,17	79,6	49,4	110,6	63,5		0,078
15000 (83.3%)	83,30%								
	100	0,245	3,23	75,5	49,7	107,4	64,1		0,078
	80	0,238	3,29	74,7	49,7	108,6	65		0,079
	70	0,222	3,42	74,6	49,6	110,8	65,9		0,081

Tab. B4 – Compressor Characterization Test – COMP50-1998

Compressor Characterization Tests 14/03/98									
FV10	FV 213	G 212	DP 201	Ti 202	Pi 298	Te out 204	Tcusc 276	Te rit 275	G 256
rpm	%	kg/s	bar	°C	bar ass	°C	°C	°C	kg/s
10000 rpm (55.5%)									
	100	0,086	0,76	69,6	25,4	75	38,6	38,8	0,027
	80	0,083	0,78	69,5	25,4	75,8	39,8	39,3	0,028
	70	0,078	0,83	69,6	25,4	76,3	40,3	39,8	0,028
	60	0,07	0,89	69,3	25,3	77,1	40,8	40,1	0,029
	50	0,058	0,96	69,2	25,2	78,4	41,4	40,2	0,030
12000 (66.6%)									
	100	0,104	1,1	69,5	25,4	82,3	45	44,1	0,033
	80	0,1	1,13	69,5	25,4	84,4	46	44,9	0,033
	70	0,094	1,18	69,5	25,4	85,7	46,7	45,5	0,034
	60	0,083	1,26	69,2	25,3	87,6	47,5	46	0,035
13000 (72.2%)									
	100	0,113	1,27	69,3	25,5	88,6	50,2	48,8	0,035
	80	0,109	1,31	69,2	25,7	90,7	53,2	51,5	0,036
	70	0,103	1,38	69,2	25,7	91,9	53,8	51,9	0,037
14000 (77.7 %)									
	100	0,122	1,49	69,2	25,8	95,8	55,8	54,1	0,039
	80	0,118	1,52	69,2	25,8	97,6	57,2	55,2	0,039
	70	0,11	1,58	69	25,6	99	57,8	55,6	0,040
15000 (83.3%)									
	100	0,131	1,7	69	25,8	101,2	59,2	57,5	0,041
	80	0,126	1,74	69,2	25,8	102,4	60,6	58,2	0,042
	70	0,118	1,81	69,2	25,8	104,2	61,4	58,9	0,043
16000 (88.8%)									
	100	0,14	1,9	69,2	25,9	106,5	62,6	60,3	0,044
	80	0,135	1,95	69	25,8	108,3	63,7	61,2	0,045
	70	0,126	2,05	68,7	25,8	111,2	64,7	62,1	0,046

Tab. B5 – Compressor Characterization Tests – COMP25-1998

Compressor Characterization Tests 14/03/98									
FV10	FV 213	G 212	DP 201	Ti 202	Pi 298	Te out 204	Tcusc 276	Te rit 275	G 256
rpm	%	kg/s	bar	°C	bar ass	°C	°C	°C	kg/s
10000 (55.5%)									
	100	0,068	0,57	71,8	23,1	81,8	43,2		0,018
	80	0,066	0,59	71,8	23,1	82,1	43		0,019
	70	0,062	0,61	71,8	23	82,3	42,9		0,019
	60	0,055	0,65	71,6	23	82,6	42,9		0,020
	50	0,046	0,7	71,6	22,9	83,5	42,9		0,020
	40	0,036	0,75	71,4	22,9	84,8	43		0,021
	30	0,024	0,83	71,2	22,8	86,4	43,4		0,022
12000 (66.6%)									
	100	0,081	0,79	71,8	22,9	88,9	46,9		0,023
	80	0,078	0,81	71,6	22,9	89,4	47,1		0,023
	70	0,073	0,85	71,8	22,8	90,1	47,2		0,023
	60	0,065	0,9	71,5	22,8	91,3	47,3		0,024
	50	0,055	0,95	71,5	22,7	93,5	47,7		0,025
	40	0,043	1,04	71,4	22,6	97	48,4		0,026
	30	0,029	1,11	71,2	22,5	101,2	49,1		0,027
13000 (72.2%)									
	100	0,087	0,92	72,1	22,8	93,3	49,8		0,024
	80	0,084	0,94	71,8	22,8	93,6	49,8		0,025
	70	0,079	0,97	71,8	22,8	95,1	50,3		0,025
	60	0,071	1,03	71,5	22,7	96,5	50,6		0,026
	50	0,059	1,1	71,5	22,7	99,6	51,2		0,027
	40	0,046	1,18	71,5	22,6	103,7	52		0,028
	30	0,031	1,3	71,1	22,5	110	53,2		0,029
14000 (77.7 %)									
	100	0,094	1,05	71,9	22,8	98	52,9		0,026
	80	0,091	1,07	71,6	22,8	98,6	53,3		0,026
	70	0,085	1,11	72,2	22,9	102,7	55,4		0,027
	60	0,076	1,18	72,1	22,8	112,5	56		0,028
	50	0,063	1,26	73,1	22,7	109,2	56,8		0,029
	40	0,05	1,37	70,5	22,6	113	56,9		0,030
15000 (83.3%)									
	100	0,101	1,2	71,8	22,9	103,6	56,8		0,028
	80	0,098	1,22	71,8	22,9	104,5	56,9		0,028
	70	0,091	1,27	71,6	22,8	105,9	57,3		0,029
	60	0,081	1,35	71,5	22,7	108,6	57,8		0,030
	50	0,067	1,45	71,2	22,6	113,5	58,8		0,031
16000 (88.8%)									
	100	0,107	1,34	72,8	22,9	108,9	58,8		0,030
	80	0,104	1,38	71,5	22,8	109,2	59,1		0,031
	70	0,101	1,43	71,4	22,8	111	59,5		0,031
	60	0,087	1,51	71,5	22,7	114	60,2		0,032

Tab. B6 – Compressor Characterization Tests – COMP25-1999